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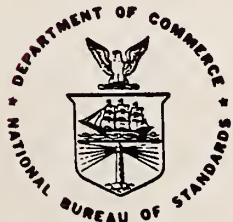
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STOVE: A Predictive Model for Heat Transfer From Solid-Fuel Appliances

Richard D. Peacock
Richard A. Dipert

U.S. DEPARTMENT OF COMMERCE
National Bureau of Standards
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Center for Fire Research
Gaithersburg, MD 20899

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U.S. DEPARTMENT OF COMMERCE, Malcolm Baldrige, *Secretary*
NATIONAL BUREAU OF STANDARDS, Ernest Ambler, *Director*

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NOMENCLATURE

F_{dA}	radiant exchange configuration factor	dimensionless
F_{12}	radiant exchange configuration factor	dimensionless
h	convection heat transfer coefficient	$\text{kW} / \text{m}^2 \cdot \text{K}$
k	thermal conductivity	$\text{kW} / \text{m} \cdot \text{K}$
L	characteristic length	m
Nu	Nusselt number	dimensionless
Pr	Prandtl number	dimensionless
R_i	thermal resistance	$\text{m}^2 \cdot \text{K} / \text{kW}$
Ra	Raleigh number	dimensionless
R_{TOTAL}	total thermal resistance = ΣR_i	$\text{m}^2 \cdot \text{K} / \text{kW}$
\dot{q}	heat transfer rate	kW/m^2
T	temperature	K
X	characteristic horizontal dimension	m
Y	characteristic vertical dimension	m
ϵ	emissivity	dimensionless
σ	Stephan-Boltzmann constant	$\text{kW} / \text{m}^2 \cdot \text{K}^4$

STOVE; A Predictive Model for Heat Transfer
From Solid Fuel Appliances

Richard D. Peacock and Richard A. Dipert

Abstract

A computer implementation of a model to predict temperatures on wall and wall protector surfaces exposed to the heating of an appliance such as a solid fuel heating appliance is described. A steady state heat transfer model with flexibility to describe a generalized method of protection for a combustible wall surface is presented along with a computer program implementing the model.

Good agreement was found comparing the model predictions with data previously collected during full scale experiments conducted to evaluate the effectiveness of generic methods of wall protection in reducing temperatures on combustible wall surfaces.

Extensive references of research related to solid fuel heating safety are included.

Key words: Chimneys; fire models; fire safety; fire tests; flues; heat transfer; heating equipment; literature reviews; radiant energy; stoves; wood.

1. INTRODUCTION

The U.S. Consumer Product Safety Commission and the U.S. Department of Energy, as part of a program to investigate safety risks involved with the use of solid fuel burning appliances, have sponsored experimental research at the Center for Fire Research (CFR) at the National Bureau of Standards (NBS) to identify hazards associated with solid fuel heating. The studies were conducted to provide information to improve safety practices for the use of the

appliances, and to provide data upon which to base improved codes and standards.

During the first years of the program, an accident survey, literature review, and codes and standards analysis were performed to establish accident patterns, to determine the types of risks involved with the use of wood burning appliances, and to ascertain the adequacy of existing codes and standards in addressing these risks [1-3].¹ Overwhelmingly, conditions related to installation, operation, and maintenance were responsible for the fire incidents studied. Only a small percentage of the fires was attributed to product design or product defects. Thus, safe installation and use of wood burning appliances is a critical requirement for preventing fire accidents involving the equipment. Much of the criteria for the installation and use of wood burning appliances are based upon data developed over forty years ago and do not provide information on materials of construction, or appliances available in the current market.

The present program at CFR includes research on:

- clearances to combustibles from appliances and chimney connectors [4];
- methods of protection to allow reduced clearances to walls and

¹

Number in brackets refer to literature references listed in section 8 at the end of this report.

ceiling surfaces exposed to radiant heating by appliances and chimney connectors [5];

- temperatures developed in and around fireplaces with and without fireplace inserts installed [6,7];
- intensity and duration of chimney fires in factory-built and masonry chimneys [8];
- temperatures on combustible material surrounding chimney connectors passing through walls and / or connecting to chimneys [9], and;
- prediction of temperatures on surfaces of combustible walls exposed to heating from a typical radiant heating appliance.

This report, one of a series of reports providing information from the experimental program on wood burning safety at NBS, presents the results of the development of a computer based implementation of a model to predict temperatures on a wall surface exposed to heating from a radiant heating appliance such as a wood stove. The resulting computer program allows the user to specify thermal protection to reduce temperatures on the wall surface.

2. REVIEW OF PREVIOUS WORK

2.1 Fire Incidents Involving Wood Burning Appliances

Recent statistics on fires and injuries related to wood burning appliances are alarming:

Year	Fires	Change From Previous Year	Deaths	Dollar Loss
1978	66,800		250	\$134 million
1979	70,700	+14%	210	\$175 million
1980	112,000	+58%	350	--
1981	130,100	+16%	290	\$265 million
1982	139,800	+7%	250	\$257 million
1983	140,600	+0.6%	280	\$296 million

Source: U.S. Consumer Product Safety Commission [10, 11]

There were more fires in solid fuel burning equipment, and a larger percentage increase over previous years, than were reported for any other kind of heating equipment -- including gas, electric, and oil burning appliances [10-11].

This marked increase is attributed to the growing installation and use of wood burning stoves in homes throughout the United States and the fact that most homes are made of combustible construction. Clearly, accidental fires from wood burning appliances are an increasingly important problem.

2.2 Clearances in Existing Codes and Standards

Recommendations for minimum acceptable clearances to combustible materials for the installation of chimney, chimney connectors, and appliances are specified in the various model building codes and recommended practices manuals. Reference [12] is typical of the specifications found in the codes. For simplicity, a single, hopefully conservative clearance is given for each type of appliance installed without protection. No allowance is made for the size, heat output, heat transfer characteristics or other features unique to individual models. Similarly, only a few, specific methods of protection employed to allow reduction of these clearances are recommended.

Typically, 0.91 m of clearance is specified between radiant heaters and unprotected combustible construction. For residential solid fuel chimneys, typically 51 mm of clearance is required. Chimney connectors for solid fuel burning residential appliances require a clearance of at least 0.46 m to combustible materials. However, as with appliances, these clearances may be reduced by the use of appropriate protection applied either to the appliance or to the combustible surface.

The experimental basis for these code requirements is not, in many cases, quite so clear. Several experimental studies have been carried out to determine minimum acceptable clearances to combustible materials. Voigt [13], in a 1933 publication, recommends a minimum clearance of 0.30 m for chimney connectors 0.23 m in diameter. A more extensive study, performed by Underwriters Laboratories in 1943 [14], presents minimum safe clearances for

both unprotected surfaces and surfaces protected by various methods. Distances at which a maximum temperature rise of 50°C above room temperature is reached are presented as a function of the temperature of the exposed face of a heat producing appliance. The relative protection afforded by various materials used as heat barriers between the appliance and combustible surfaces is also examined. Lawson, Fox, and Webster [15] and Lawson and Simms [16] have studied the heating of wall panels and wood by radiation. With experimentation and theoretical predictions, they present safe clearances between flue pipes and wall surfaces as a function of the pipe diameter and the pipe surface temperature. To maintain a maximum wall temperature of 100°C , 0.15 m pipe should not exceed 350°C in surface temperature at a clearance of 0.46 m [15]. Loftus and Peacock [5] present the results of research studying clearances and methods of protection for wall and ceiling surfaces exposed to radiant heating appliances. A number of recommended methods of protection to reduce temperatures on combustible wall and ceiling surfaces to acceptable levels were found. In the study, appliance surface temperatures from 300 to 450°C were used.

These experimental studies established limits for two important parameters: appliance surface temperature and clearance to combustibles for unprotected and protected surfaces. Maximum appliance surface temperatures for the appliances studied ranged from 300 to 450°C ; average appliance surface temperatures from 200 to 250°C . Minimum safe wall clearances for unprotected surfaces ranged from 0.31 to 0.91 m. Most of the current code provisions are only adequate for maximum appliance surface temperatures up to 300 to 350°C .

2.3 Temperatures Developed in Heating Systems

Tests made with prefabricated porcelain-enameled metal chimneys for solid or liquid fuel furnaces [17,18] established a limiting temperature rise of 190°C on the outer surface of the chimney for a flue gas temperature of 537°C . With this limitation, wood framing space 51 mm or more away from the chimney was considered safe. Satisfactory insulation of the chimneys to reduce the outer surface temperatures to acceptable levels was obtained with asbestos paper plies totalling about 45 mm in thickness. In the same study, some asbestos cement pipe coverings were also found to reduce heat transmission to the extent required for safety of nearby combustibles.

To establish performance requirements for lightweight prefabricated chimneys, tests were conducted with lined and unlined masonry chimneys having 102 mm thick walls [19,20]. Hazardous conditions on wood framing spaced 51 mm away from the chimney were noted with a continuous flue gas temperature of 482°C for the unlined chimney and 592°C for the lined chimney. However, these hazardous conditions were not reached in the lined chimney tests until after 13 hours. In order to study operating conditions with typical fuels, a number of firing tests [21] were conducted with heating appliances known to give high flue gas temperatures, using wood and soft coals as fuels. With a coal-fired, jacketed type heater, gas temperatures ranging from 648 to 704°C were measured for an hour or more in the flue at the ceiling level above the heater.

Lawson, Fox, and Webster [15] presented results of tests to measure surface temperature of flue pipes. Measured for a variety of flue systems using solid fuels -- mostly coal and coke -- they report temperatures of about 150°C under "normal" conditions and temperatures as high as 815°C for over fire conditions.

Fox and Whittaker [21] report temperatures on metal flues of several heating appliances operated over a range likely to encountered in normal use. Maximum flue pipe surface temperatures ranged from 704 to 815°C at the appliance flue outlet, 360 to 510°C at a distance of 0.91 m from the appliance flue outlet, and 287 to 326°C at a distance of 1.8 m from the appliance flue outlet.

Shoub [17] concluded that combustible materials will be ignited if maintained in continued contact with a masonry chimney of 120 mm wall thickness with flue gas temperatures of 400°C.

In tests for the Department of Energy [4], temperatures ranging from 297 to 436°C during normal operation and 377 to 693°C during over fire conditions were noted on the surfaces of several wood burning appliances when tested to prescribed test methods [22]. A total of 11 different short term tests, ranging from 1.9 to 25.6 hours duration, were conducted to establish normal firing conditions in wood burning appliances [23]. An examination of the data from these tests shows spikes occurring at the beginning and end of tests and, apparently, whenever the door to the stove was opened. These sharp increases in temperature were attributed to a "high fire" in the morning and to

the rapid increase in active flaming when the door was opened for refueling the fire. The average stove surface temperature rise for normal burning ranged from 177 to 218°C, flue gases from 140 to 269°C, inner chimney wall surface 119 to 241°C, and the outer chimney wall surface 14 to 48°C.

2.4 Limiting Safe Temperatures on Combustible Surfaces

Listings of heat producing appliances and methods for setting clearances between appliances and combustible surfaces are based upon Underwriters Laboratories listings [22]:

- maximum temperature rise of 65°C above room temperature on exposed surfaces; and
- maximum temperature rise of 50°C above room temperature on unexposed surfaces, such as beneath the appliance, floor protector, or wall mounted protective device.

These requirements are based upon the fact that while the ignition temperature of wood products is generally quoted to be on the order of 200°C [24], wood that is exposed to constant heating over a period of time may undergo a chemical change resulting in a much lowered ignition temperature and increased potential for self-ignition.

Mitchell [25] presents data on wood fiberboard exposed to temperatures as low as 109°C that resulted in ignition after prolonged exposure. MacLean

[26,27] reports charring of wood samples at temperatures as low as 93°C. He concludes that wood should not be exposed to temperatures appreciably higher than 66°C for long periods. McGuire [28] suggests that the maximum safe temperatures on the surface of a combustible material adjacent to a constant heat source should be no more than 100°C.

Clearly, the ignition of wood at moderately elevated temperatures is a complex phenomenon; the time of exposure is indeed an important parameter [29,30]. While exact limits recommended in the literature vary due to exposure time and details of the tests conducted, the numerous documented fires involving the ignition of wood members near low pressure steam pipes [31] suggest an upper temperature limit for wood exposed to long-term low-level heating should not be appreciably higher than 100°C.

Nearby combustible materials other than wall and ceiling surfaces, such as chairs or draperies must also be kept a sufficient distance from combustible materials to prevent ignition of the materials. The testing standards and model codes treat all combustibles with the same requirements. Thus, the 0.91 m clearance requirements in NFPA 211 and maximum temperature rise requirements in the Underwriters Laboratories testing standards apply equally well to other combustibles as well. Similarly, a temperature limit of 100°C is more than adequate to protect most combustibles used in furnishings.

2.5 Data for Model Validation

Much of the available literature related to wood heating safety provides a significant amount of data that can be used to compare theoretical predictions with experimental measurements. In the above literature, references [4], [5], and [9] provide measurements of appliance surface temperatures and wall surface temperatures and provide a full description of the experimental setup to be modeled. Reference [22] provides acceptable limits on combustible surface temperatures for use in predicting minimum clearances, maximum appliance surface temperatures, minimum acceptable protector thermal properties, and the like. These references will provide the majority of data for the comparison of theoretical predictions with measured temperatures on surfaces of appliances, on protector systems, and on combustible walls.

3. THEORETICAL BASIS FOR THE MODEL

Figure 1 presents a schematic diagram of a heating appliance / wall system with an arbitrary protection system between the appliance and the wall. Heat transfers from the hot stove surface through any intervening protection to the wall surface, through the wall, and to the cooler surroundings. A few assumptions, reasonable to the system being modeled, simplify the model considerably:

- The stove is operating at steady state conditions (thus, we assume the stove has been operating for a period of time and has reached a steady operating condition).
- Stove is at a constant uniform surface temperature.
- Heat transfer through air spaces in the system takes place by radiation and convection only.
- Heat transfer through solids in the system takes place by conduction only.

With these assumptions, a one-dimensional, steady state model of the stove / protector / wall heat transfer is appropriate. The only loss in generality of the predictive capability of the model is the inability to predict any time dependent behavior of the system. Since the intended purpose of the model is to study the fire safety of the stove / protector / wall system under worst case conditions, this loss is acceptable. By assuming steady state conditions with a constant stove temperature, the worst case conditions will be modeled.

3.1 Radiative Heat Transfer

For heat exchange between two surfaces, the net radiative heat transfer between surfaces 1 and 2 is given by [32]:

$$\dot{q} = \frac{\sigma (T_1^4 - T_2^4)}{\frac{1 - \epsilon_1}{\epsilon_1} + \frac{1}{F_{12}} + \frac{1 - \epsilon_2}{\epsilon_2}} \quad (1)$$

F_{12} , the configuration factor for radiative exchange between surface 1 and surface 2, is defined as the fraction of the radiation leaving surface 1 which is intercepted by surface 2. Compilations of configuration factors are available in the literature [33,34]. For the stove / wall protector geometry, the following equations are appropriate. The configuration factor for a differential element to a plane parallel rectangle with the normal to the element passing through the corner of the rectangle is given by [33]:

$$F_{dA} = \frac{1}{2\pi} \left[\frac{X}{(1+X^2)^{1/2}} \tan^{-1} \frac{Y}{(1+X^2)^{1/2}} + \frac{Y}{(1+Y^2)^{1/2}} \tan^{-1} \frac{X}{(1+Y^2)^{1/2}} \right] \quad (2)$$

where $X = (\text{width of rectangle}) / (\text{distance from rectangle to element})$ and $Y = (\text{height of rectangle}) / (\text{distance from rectangle to element})$. Since the configuration factor for a surface equals the sum of configuration factors for any subdivision of the surface, the configuration factor for any point (X_w, Y_w) on the wall (or first protector) surface can be defined from equation (2) as

$$F_{12} = F_{dA}(X_W - X_S, Y_W - Y_S) - F_{dA}(X_W - X_S - W_S, Y_W - Y_S) + \\ F_{dA}(X_W - X_S - W_S, Y_W - Y_S - H_S) - F_{dA}(X_W - X_S, Y_W - Y_S - H_S) \quad (3)$$

For radiant heat exchange between two identical, directly opposed rectangles (such as two protective surfaces of the same size), the configuration factor is given by [33]

$$F_{12} = \frac{2}{\pi XY} \left[\ln \left[\frac{(1+X^2)(1+Y^2)}{1 + X^2 + Y^2} \right]^{\frac{1}{2}} + X(1+Y^2)^{\frac{1}{2}} \tan^{-1} \frac{X}{(1+Y^2)^{\frac{1}{2}}} \right. \\ \left. + Y(1+X^2)^{\frac{1}{2}} \tan^{-1} \frac{Y}{(1+X^2)^{\frac{1}{2}}} - X \tan^{-1} X - Y \tan^{-1} Y \right] \quad (4)$$

3.2 Convective Heat Transfer

For convective heat transfer between two surfaces separated by an air space, the net heat exchange by convection is given by

$$\dot{q} = h (T_1 - T_2) \quad (5)$$

where h is the convective heat transfer coefficient. For free convection at

the surface of a vertical surface (such as the wall, appliance, or protector surface), h can be found from the equations [35]

$$Nu_L = \frac{h L}{k} = \left[0.825 + \frac{0.387 Ra_L^{1/6}}{\left[1 + (0.492/Pr)^{9/16} \right]^{8/27}} \right]^2 \quad (6)$$

3.3 Conductive Heat Transfer

For solids, the net heat exchange by conduction is given by

$$\dot{q} = \frac{k}{L} (T_1 - T_2) \quad (7)$$

While for some materials, the thermal conductivity, k , is a function of temperature, for most materials, the assumption that k is a constant leads to inconsequential loss in generality. For instance, for aluminum, the thermal conductivity changes by only 25% over a temperature range from -170°C to well over 2000°C

3.4 Solution of the Equations for an Arbitrary Protection System

At steady state, the heat transferred from the appliance to the outside, figure 2, is equal to the heat transferred through any element or group of elements within the system, or

$$\dot{q}_{\text{TOTAL}} = \frac{(T_S - T_O)}{R_{\text{TOTAL}}} = \dot{q}_i = \frac{(T_i - T_{i+1})}{R_i} \quad (8)$$

Equations (1), (5), and (7) can be expressed as in equivalent resistance forms as

$$\text{(Conduction)} \quad R_i = \frac{L}{K} \quad (9)$$

$$\text{(Convection)} \quad R_i = \frac{1}{h} \quad (10)$$

$$\text{(Radiation)} \quad R_i = \frac{\frac{1 - \epsilon_1}{\epsilon_1} + \frac{1}{F_{12}} + \frac{1 - \epsilon_2}{\epsilon_2}}{\sigma (T_1^2 + T_2^2) (T_1 + T_2)} \quad (11)$$

For the current problem, these equations can be combined into two as

$$\text{(Solids)} \quad R_i = \frac{L}{K} \quad (12)$$

$$(Airsapces) \quad R_i = \frac{1}{\frac{1}{h} + \frac{\sigma (T_1^2 + T_2^2) (T_1 + T_2)}{\frac{1 - \epsilon_1}{\epsilon_1} + \frac{1}{F_{12}} + \frac{1 - \epsilon_2}{\epsilon_2}}} \quad (13)$$

Thus, the solution method with a given appliance temperature, T_s , and a given temperature of the surroundings, T_o , begins by assuming temperatures for the intermediate surfaces, calculating individual resistances from equations (12) and (13) to determine the total resistance, R_{TOTAL} , calculating the total heat flow rate from equation (8), and comparing the total heat flow rate to the individual heats. If the calculated individual rates are sufficiently close to the calculated total heat flow rate, the steady state solution has been obtained. If any of the individual heats are different from the total heat, new estimates for each of the intermediate temperatures are made and the process is repeated until sufficient agreement has been found. Reference [36] provides a number of methods for making best guess estimates for the next iteration toward the solution. For the current problem, a simple linear search is used where one variable at a time is changed until a local optimum is found.

A number of literature sources are available to allow determination of the physical data required for the input (for instance, for the thermal conductivity and emissivity). References [32] and [33] provide extensive listings of thermal and material properties for common materials.

4. COMPUTER IMPLEMENTATION OF THE MODEL

Included as Appendix A is a listing of the FORTRAN (written in ANSI standard FORTRAN 77) program implementing the model as described above. The general structure of the program is illustrated in figure 3.

Program input (detailed in Appendix B) takes the form of different key words with arguments to specify values which depend upon the key word. In most cases, the order of the key words is unimportant. A description of each of the input key words and values which go on the same line are presented below:

STOVE	<height> <width> <emissivity> <temperature>
AIRSPACE	<thickness> <emissivity>
FOR	<variable> = <lower> <upper> <increment>
XWALL	<x position>
YWALL	<y position>
PROTECTOR	<thickness> <height> <width> <k> <emissivity> <temperature>

A sample input for the program follows:

```

FOR:          TSTOVE = 473.15 673.15 10.
STOVE:        0.9 0.5 0.5 473.15
AIRSPACE:     0.91 0.9
ALUMINUM SHEET: 0.00254 3.0 3.0 177. 0.9
AIRSPACE:     0.0254 0.9
ALUMINUM SHEET: 0.00254 3.0 3.0 177. 0.9
AIRSPACE:     0.0254 0.9
GYPSUM WALLBOARD: 0.0127 3.0 3.0 0.17 0.9
F/G INSULATION: 0.0916 3.0 3.0 0.038 0.9
BRICK OUTSIDE: 0.0916 3.0 3.0 0.72 0.9
AIRSPACE:     273.15
END:

```

This input specifies a series of calculations to be done for a stove temperature ranging from 200°C to 400°C (473.15 to 673.15 K in the input above) for a wall protection system consisting of two aluminum sheets spaced 25 mm (0.00254 m in the input above) apart and placed 25 mm from an insulated outside wall of a house. A clearance of 0.91 m from the appliance to the first aluminum sheet is specified. A sample output from the program, using this sample data set, is presented in table 1. Calculated temperatures on all surfaces from the stove to the outdoors are shown along with the specified sizes and thermal properties of the materials used for the walls and protectors. Execution time, of course, depends upon the computer in use. On a typical desk top personal computer, execution of the above test case required less than 1.5 minutes.

5. COMPARISON OF THE MODEL PREDICTIONS WITH EXPERIMENTAL DATA

Figure 4 presents a comparison of calculated temperatures on the surfaces of wall protectors and on the surfaces of combustible walls with experimentally measured values taken from references [4] and [5]. To assess the predictive capabilities of the model, a range of conditions from the experimental studies were simulated. Wall materials used in these experimental studies ranged from uninsulated gypsum wallboard to a fully insulated stud wall with a brick facing on the exterior. A number of different wall protection methods were taken from reference [5], varying from a simple sheet metal protector to a sheet metal / insulation board / air space composite protector or a ventilated brick protector. A simple cross plot of

the calculated values and the experimental values illustrates the agreement of the model's predictions with experimental data obtained in earlier studies. Agreement of the calculated values with the experimentally measured values, stated as

$$\left(\left(T_{\text{calculated}} - T_{\text{measured}} \right) / T_{\text{calculated}} \right) * 100$$

with temperatures expressed in absolute, averaged within less than 1 percent. Individual agreement, however ranged from 5 percent low (calculated values lower than experimental) to 4 percent high. Much of the disparity in the comparison can be explained by the choice of ambient conditions for the experimental tests. All the data in the two reports were described in terms of temperature rise above ambient conditions. Since the experimental calculations are based upon absolute temperatures, some assumptions had to be made for the ambient temperatures in the surroundings during the tests. A variation in ambient temperature of 15°C could change the calculated surface temperatures on the wall surfaces by as much as ±10 percent. Thus, the agreement illustrated in figure 5 is excellent in light of the possible variation in the calculations depending upon the assumed ambient temperature.

6. MODEL CAPABILITIES AND EXAMPLES

A theoretical model for predicting the heat transfer between the appliance and the wall surfaces can be a useful tool not only in the design of appliances and wall protection devices but also in the design of future experiments to study clearances and reduced clearances for wood burning

appliances. This section presents some examples of the use of the model in predicting temperatures and clearances from combustibles for both protected and unprotected wall surfaces.

6.1 Heat Transfer From Appliance to an Unprotected Wall

Figure 5 shows calculated wall surface temperatures as a function of appliance / wall clearance for a medium size appliance (an appliance 0.5 by 0.5 m on the side parallel to the wall surface) adjacent to an unprotected wall surface for appliance surface temperatures from 150 to 350°C. For these calculations, the outside air temperature (temperature of the surroundings) was assumed equal to 0°C. The wall consisted of 12 mm gypsum wallboard, a 92 mm stud space with glass fiber insulation, and a 92 mm common brick facing on the outside of the wall exposed to the outdoors. At an appliance clearance of 0.91 m, appliance surface temperatures greater than about 300 °C would lead to temperatures on the wall in excess of the recommended limit [22] of 50°C above room ambient temperature at a point on the wall directly centered behind the appliance. Since, in an earlier study [4], average appliance surface temperatures of about 200 °C were noted, a sufficient margin of safety is indicated for an appliance this size.

6.2 Heat Transfer From Appliance to a Sheet Metal Protected Wall

Figures 6 and 7 show calculated wall surface temperatures as a function of appliance / wall clearance for a medium size appliance (an appliance 0.5 by 0.5 m on the side parallel to the wall surface) adjacent to a protected wall surface for appliance surface temperatures from 150 to 350°C. As before, the outside air temperature was assumed equal to 0°C. The wall protector consisted of two sheets of aluminum (2.5 mm in thickness) separated by a ventilated 25 mm air space. The wall protector was spaced from the wall by a ventilated 25 mm air space. The wall consisted of 12 mm gypsum wallboard, a 92 mm stud space with glass fiber insulation, and a 92 mm common brick facing on the outside of the wall exposed to the outdoors. With the surfaces of the protector painted black and at an appliance clearance of 0.91 m, appliance surface temperatures greater than about 300°C would lead to temperatures on the wall in excess of the recommended limit of 50°C above room ambient temperature -- in fact, about the same as the case with no protection. However, when the surfaces of the protector are left unpainted (shiny aluminum surfaces), appliance surface temperatures higher than 350°C are required to raise the temperature of the wall surface above acceptable limits. Conversely, the clearance of the appliance to the wall could be reduced from 0.91 m to 0.3 m with an average appliance surface temperature of 200°C.

6.3 Heat Transfer From Appliance to a Masonry Protected Wall

Figure 8 shows calculated wall surface temperatures as a function of appliance / wall clearance for the same appliance (an appliance 0.5 by 0.5 m on the side parallel to the wall surface) adjacent to a protected wall surface for appliance surface temperatures from 150 to 350°C. Again, the outside air temperature was assumed equal to 0°C. The wall protector consisted of a 92 mm thick solid brick wall was spaced from the wall by a ventilated 25 mm air space. The wall consisted of 12 mm gypsum wallboard, a 92 mm stud space with glass fiber insulation, and a 92 mm common brick facing on the outside of the wall exposed to the outdoors. With the surfaces of the protector painted black and at an appliance clearance of 0.91 m, appliance surface temperatures greater than about 300°C would lead to temperatures on the wall in excess of the recommended limit of 50°C above room ambient temperature -- again not significantly lower than in wall surface temperatures than for the unprotected wall. Note, however, one of the major thermal characteristics of a masonry wall protection system -- high thermal mass -- is not accounted for in a steady state prediction.

7. USES FOR AND LIMITATIONS OF THE MODEL

A model was developed to predict temperatures on protected and unprotected wall surfaces exposed to heating from a (primarily) radiant heating appliance. A one-dimensional, steady state model of appliance / protector / wall heat transfer showed agreement within an average of less than 1 percent

when compared to experimental results from earlier laboratory studies. A range of building materials typical of residential construction, along with a number of different wall protection methods were simulated in the comparison. As a guideline to the range of applicability of the model, the variations of the thermal properties used in the comparisons were

k:	0.038	to	177	W/m · K
ε:	0.1	to	0.9	
airspace thickness:	0.1	to	1.0	m
solid thickness:	0.0025	to	0.1	m

Improvements in the program implementation of the model are possible. The simple linear search for the solution of the equations is certainly not the most efficient method. A number of search methods have been described in the literature [36]. An n-dimensional simplex search where the next guess for a given variable depends upon the values of the other n-1 variables would improve the execution speed of the program. Additional improvements would be realized with any of a number of acceleration methods, also available in the literature [36]. Of course, a more complicated, harder to understand and modify program would result.

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Table 1. Sample Output From STOVE

DOUBLE ALUMINUM PLATE, ALL SURFACES PAINTED BLACK

NUMBER OF NODES IN CALCULATION: 10

POINT ON WALL: (X): 0.000 (Y): 0.000

SERIES OF CALCULATIONS FOR VARIABLE TSTOVE: 473.150 673.150 20.000

I	MATERIAL	HEIGHT (m)	WIDTH (m)	THICK (m)	EMISS	K (W/m·K)	TEMPERATURE (°C)
0	STOVE	0.50	0.50		0.90		200.00
1	AIRSPACE			0.91	0.90		
2	ALUMINUM SHEET	3.00	3.00	0.00	0.90	177.000	
3	AIRSPACE			0.03	0.90		
4	ALUMINUM SHEET	3.00	3.00	0.00	0.90	177.000	
5	AIRSPACE			0.03	0.90		
6	GYPSUM WALLBOARD	3.00	3.00	0.01	0.90	0.170	
7	INSULATION	3.00	3.00	0.09	0.90	0.038	
8	BRICK OUTSIDE	3.00	3.00	0.09	0.90	0.720	
9	AIRSPACE			0.00	1.00		0.00

- 0: STOVE / AIRSPACE
- 1: AIRSPACE / ALUMINUM SHEET
- 2: ALUMINUM SHEET / AIRSPACE
- 3: AIRSPACE / ALUMINUM SHEET
- 4: ALUMINUM SHEET / AIRSPACE
- 5: AIRSPACE / GYPSUM WALLBOARD
- 6: GYPSUM WALLBOARD / INSULATION
- 7: INSULATION / BRICK OUTSIDE
- 8: BRICK OUTSIDE / AIRSPACE
- 9: AIRSPACE

TSTOVE	(0) (°C)	(1) (°C)	(2) (°C)	(3) (°C)	(4) (°C)	(5) (°C)	(6) (°C)	(7) (°C)	(8) (°C)	(9) (°C)
473.150	200.0	33.1	33.1	31.6	31.6	30.1	29.3	3.1	1.7	0.0
493.150	220.0	38.7	38.7	37.0	37.0	35.3	34.4	3.6	2.0	0.0
513.150	240.0	44.7	44.7	42.8	42.8	41.0	39.9	4.2	2.3	0.0
533.150	260.0	51.1	51.1	49.0	49.0	47.0	45.7	4.7	2.6	0.0
553.150	280.0	57.8	57.8	55.6	55.6	53.4	51.9	5.4	2.9	0.0
573.150	300.0	64.8	64.8	62.5	62.5	60.1	58.5	6.0	3.2	0.0
593.150	320.0	72.2	72.2	69.7	69.7	67.2	65.4	6.7	3.6	0.0
613.150	340.0	79.9	79.9	77.3	77.3	74.6	72.6	7.4	3.9	0.0
633.150	360.0	87.8	87.8	85.1	85.1	82.3	80.1	8.1	4.3	0.0
653.150	380.0	96.0	96.0	93.2	93.2	90.3	87.8	8.8	4.7	0.0
673.150	400.0	104.3	104.3	101.5	101.5	98.5	95.8	9.6	5.0	0.0

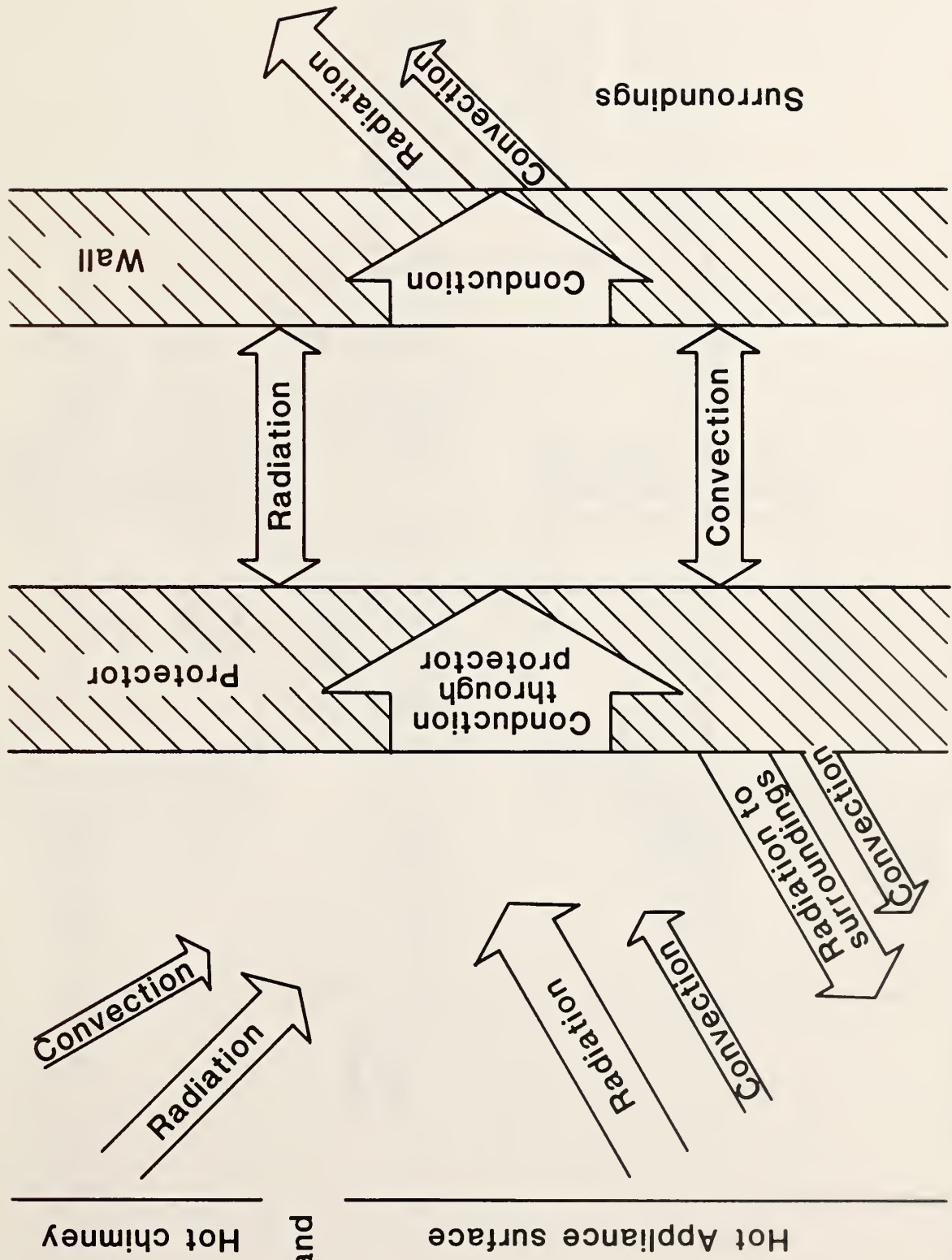


Figure 1. Heat Transfer From Hot Appliance to Cooler Wall Surface

Figure 2. Node Model Representation of Stove / Protector / Wall System

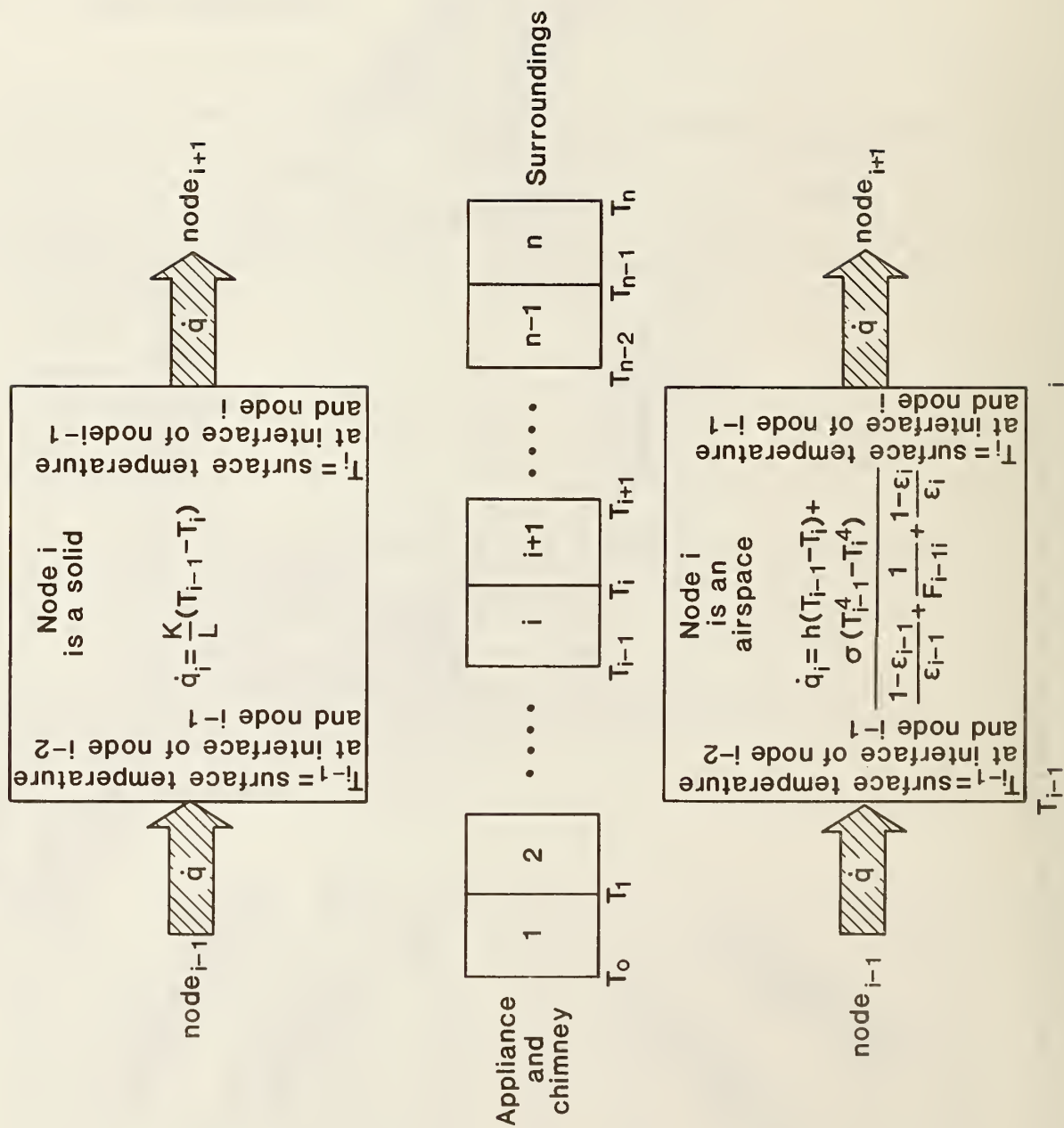


Figure 3. Program Layout For Program STOVE

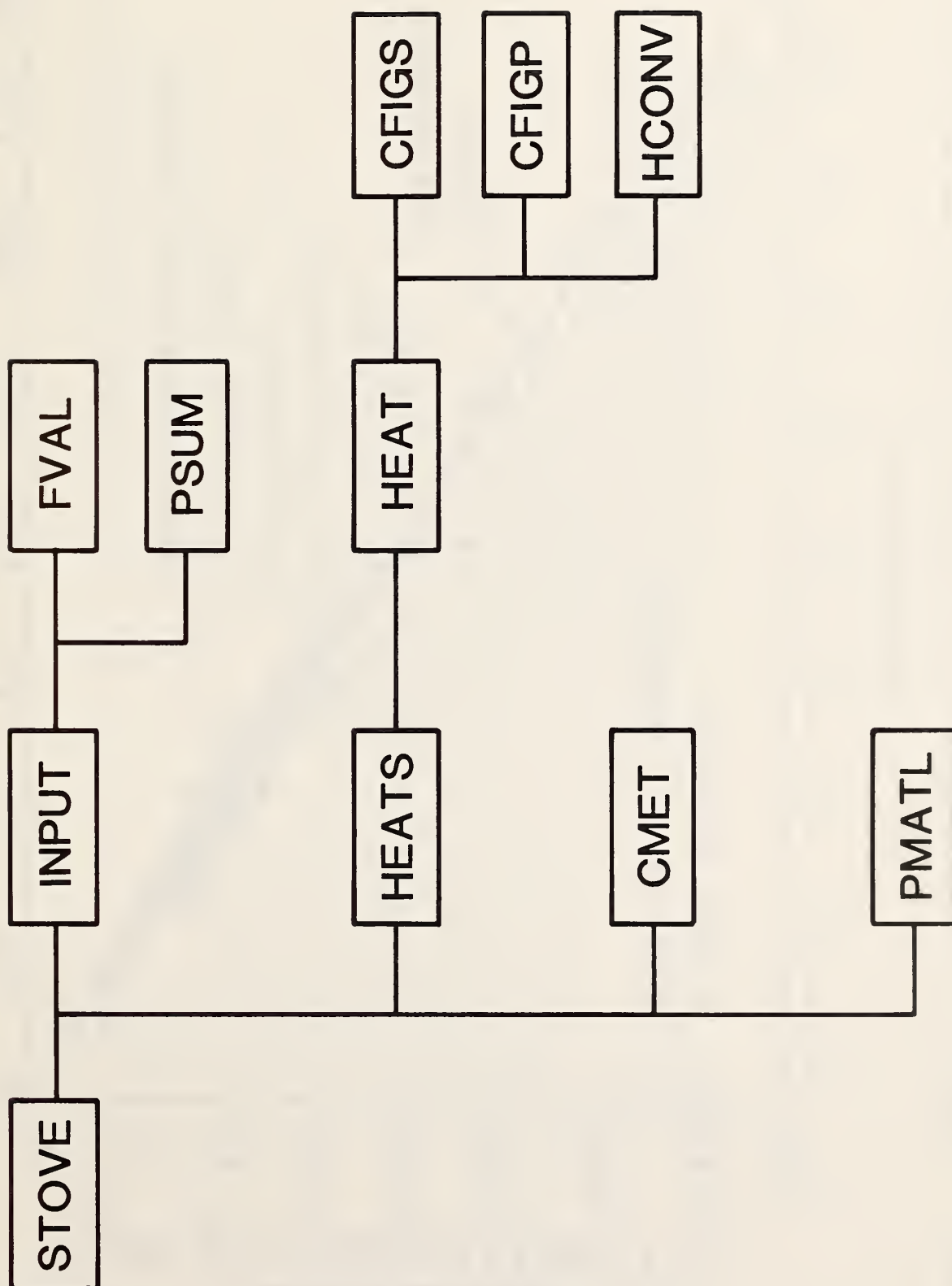


Figure 4. Comparison of Calculated Wall and Protector Surface Temperatures With Experimental Results

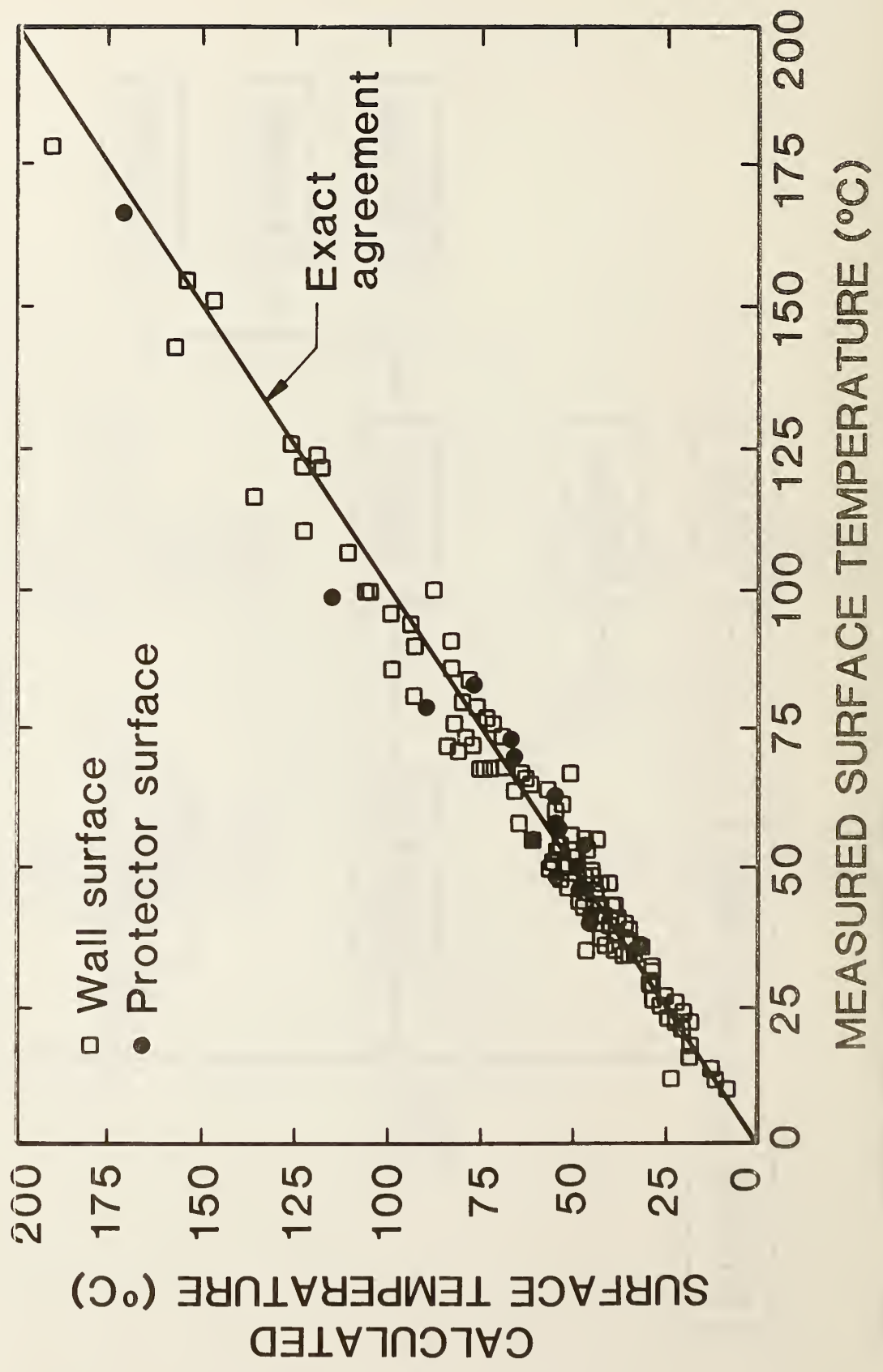


Figure 5. Predicted Wall Surface Temperatures for Heat Transfer From Appliance Surface to an Unprotected Combustible Wall Surface

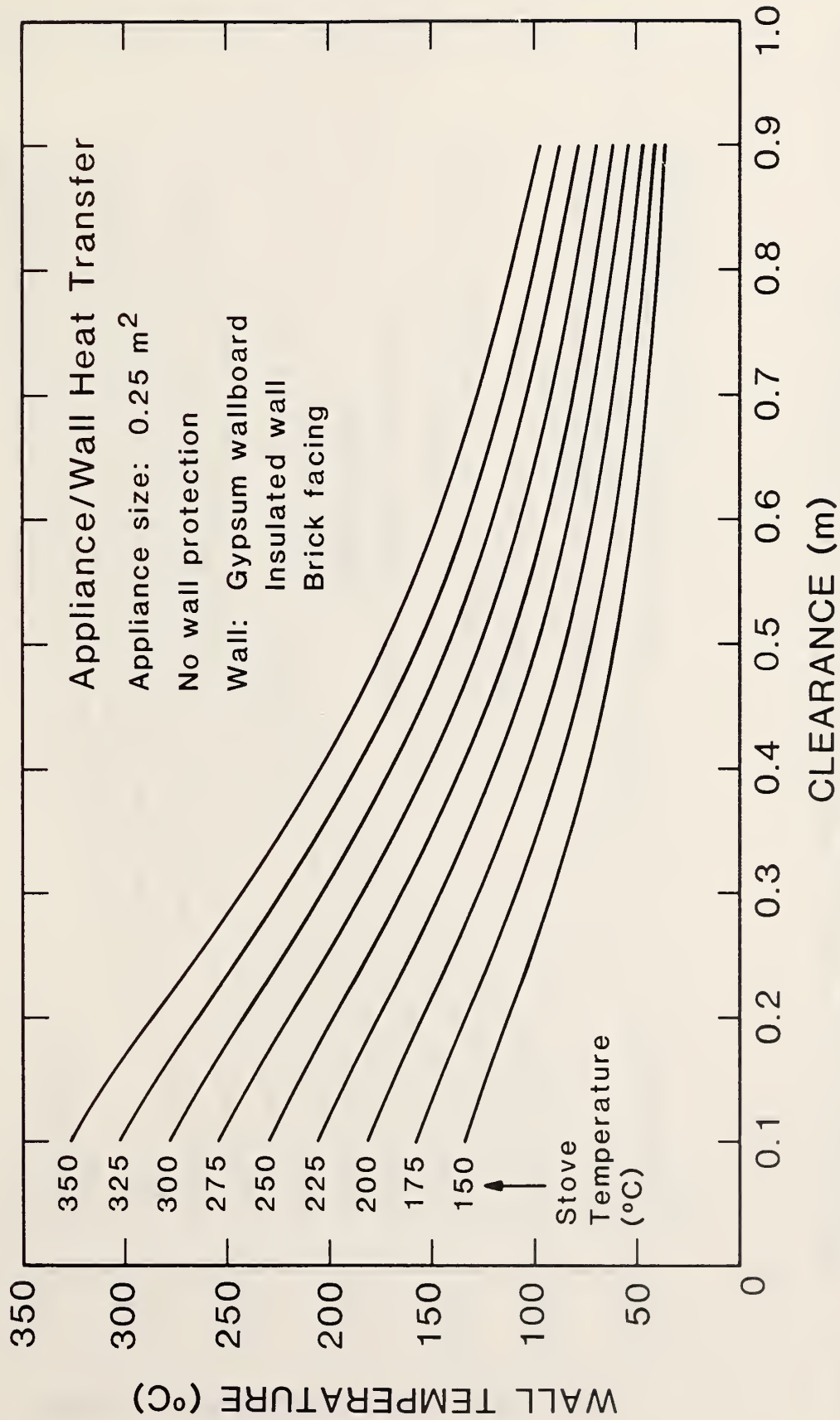


Figure 6. Predicted Wall Surface Temperatures for Heat Transfer From Appliance Surface to a Combustible Wall Protected With a Double Aluminum Sheet Wall Protector (Painted Black)

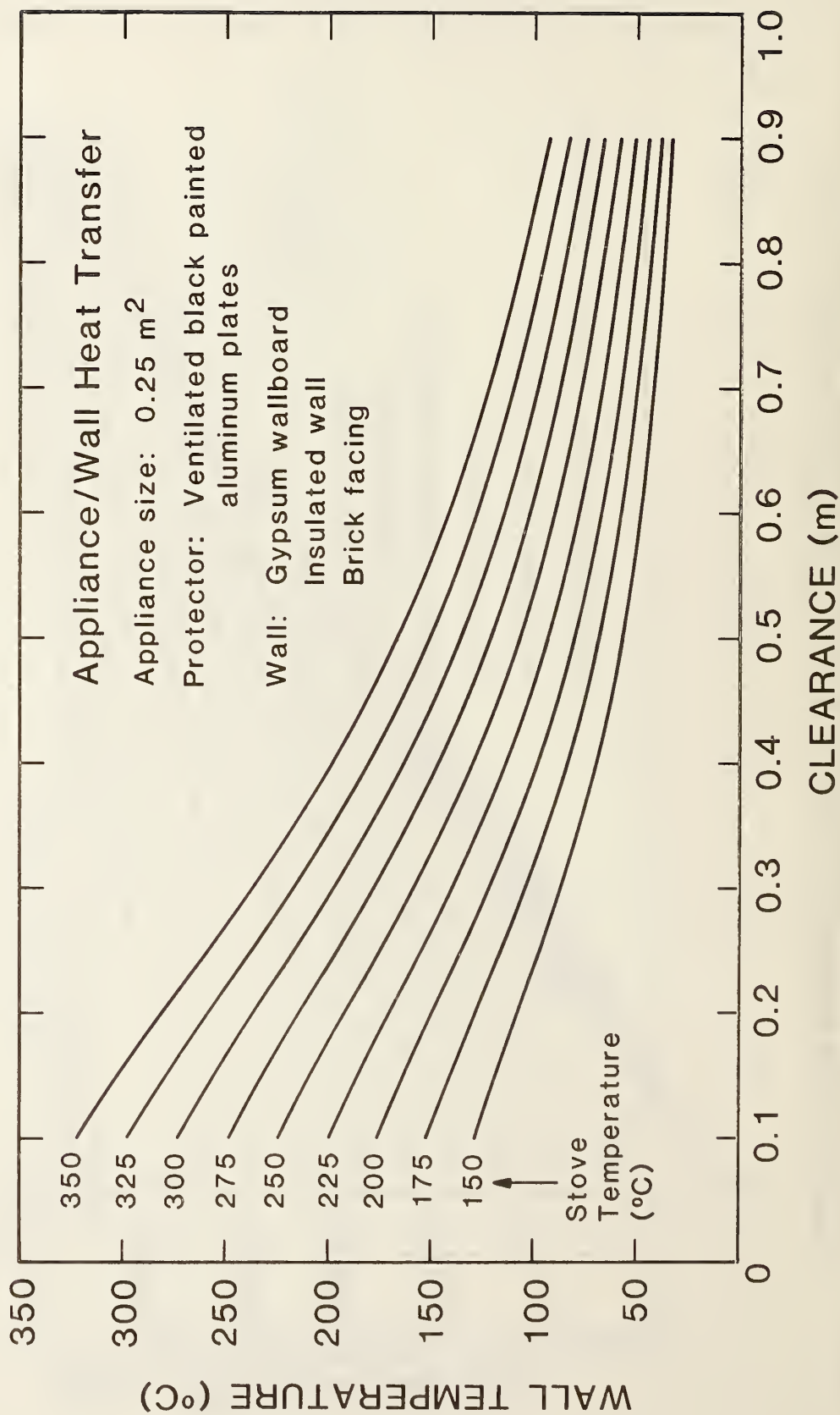


Figure 7. Predicted Wall Surface Temperatures for Heat Transfer From Appliance Surface to a Combustible Wall Protected With a Double Aluminum Sheet Wall Protector

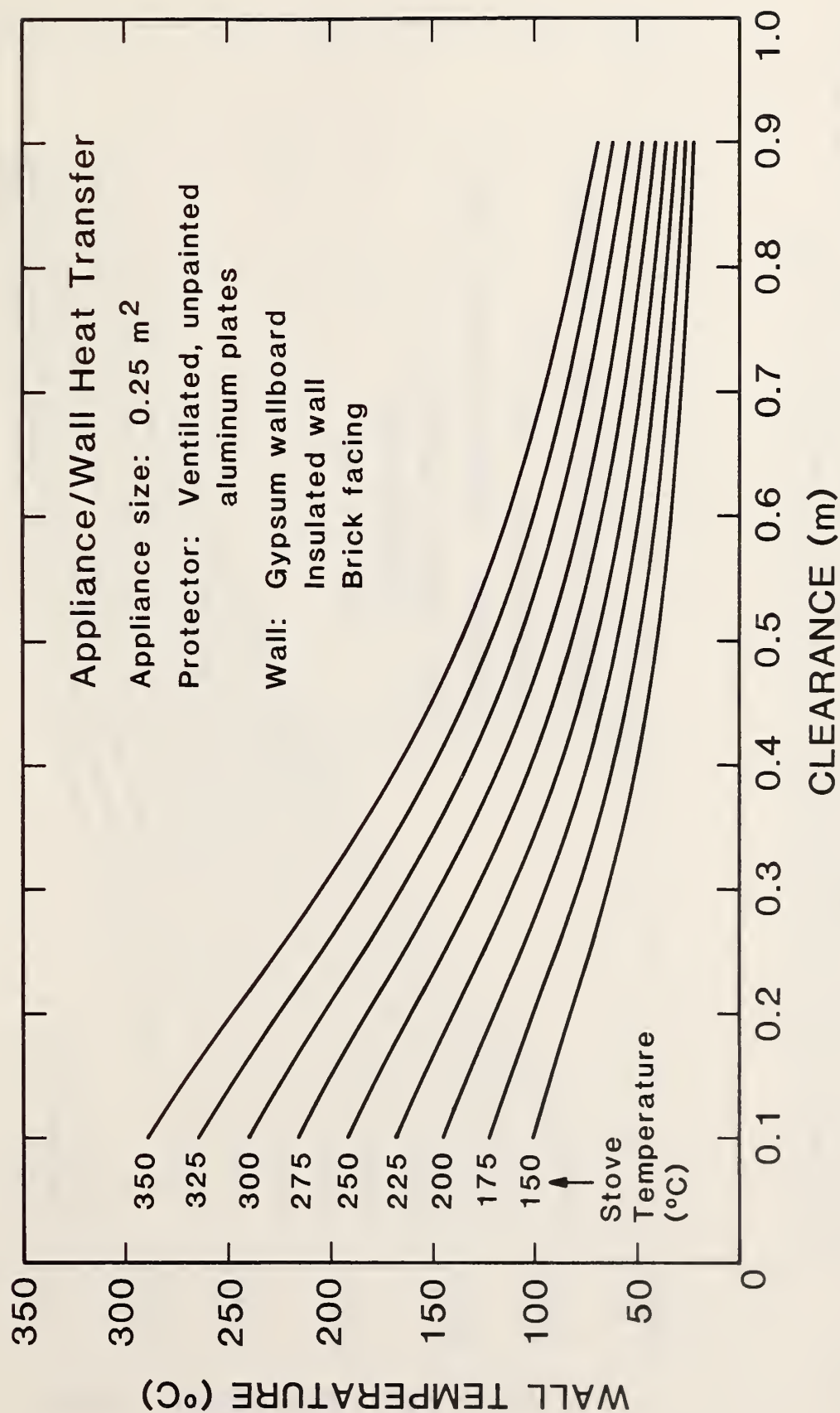
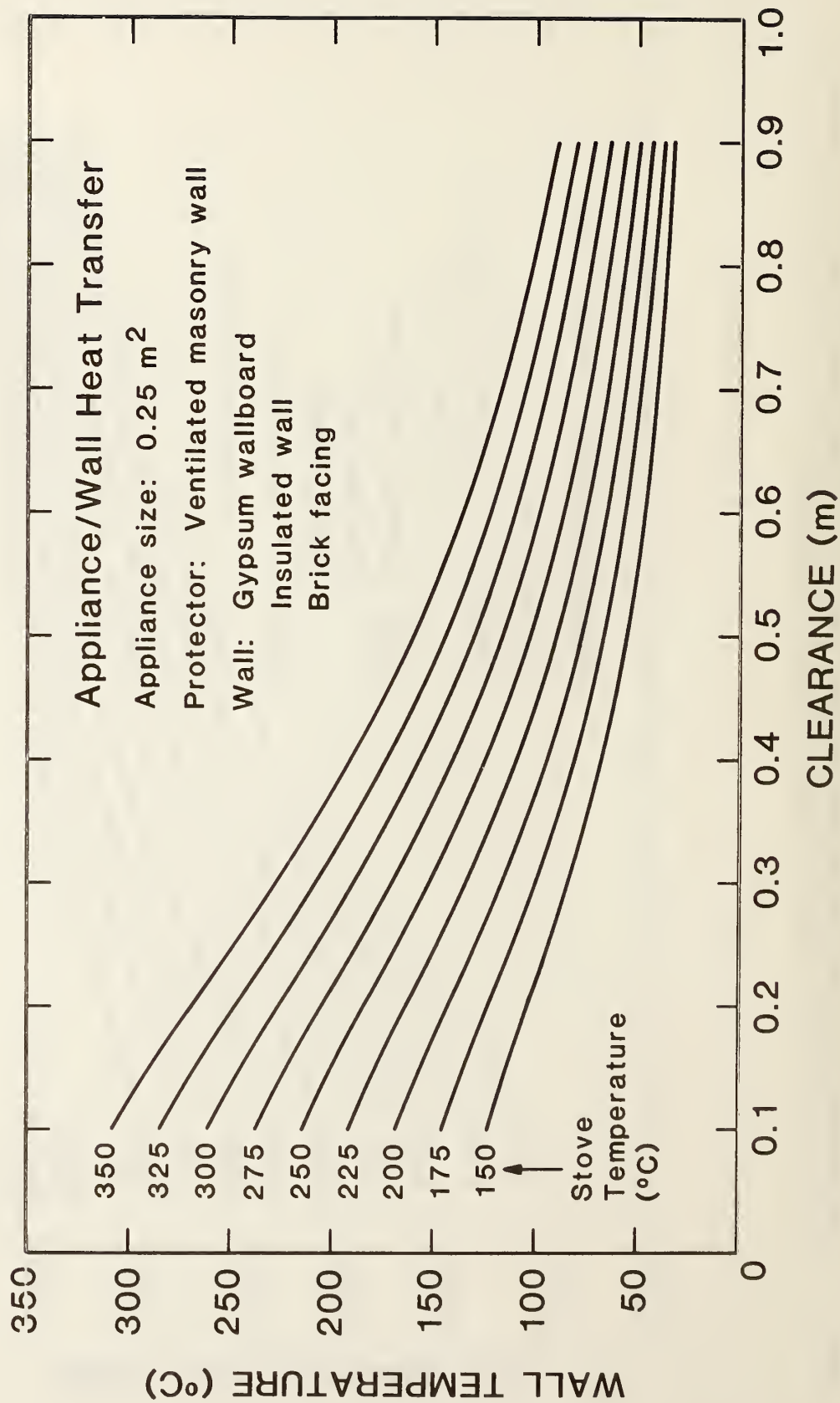


Figure 8. Predicted Wall Surface Temperatures for Heat Transfer From Appliance Surface to a Combustible Wall Protected With a Solid Masonry Wall Protector With A Ventilated Air Space



Appendix A: Program Listing of STOVE


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1 | PROGRAM STOVE
2 | C
3 | C
4 | C
5 | C
6 | C
7 | C
8 | C
9 | C
10 | C
11 | C
12 | C THIS PROGRAMS CALCULATES AN ENERGY BALANCE ON A STOVE / WALL SYSTEM
13 | C ASSUMING STEADY STATE CONDITIONS, WITH AN ARBITRARY NUMBER OF WALL
14 | C PROTECTORS BETWEEN THE STOVE AND THE WALL
15 | C
16 | C INCLUDE 'STOVE.CMN'
17 | C CHARACTER CMET*5,PMATL*60,VERSN*7
18 | C LOGICAL THRU1,NOTYET,THEEND
19 | C DATA VERSN /'86.0108'/
20 | C
21 | C INITIALIZE EVERYTHING TO DEFAULT CONDITIONS, READ INPUT FOR CASE
22 | C
23 | C QEPS=0.00001
24 | C EPS=0.0001
25 | C TSTEP1=2.
26 | C TSTEP2=2.
27 | 10 CALL INPUT(THEEND)
28 | C IF (.NOT. THEEND) THEN
29 | C XSTOVE=WSTRVE/2.
30 | C YSTOVE=0.
31 | C IF (.NOT.FULPRT) THEN
32 | C WRITE (6,11) (I,PMATL(MATL(I),MATL(I+1)),I=0,N-1),N,MATL(N)
33 | C WRITE (6,12) VNAME,(I,I=0,N)
34 | C WRITE (6,8) ' ',(' (°C) ',I=0,N)
35 | C WRITE (6,8) ('-----',I=-1,N)
36 | C END IF
37 | C NCALCS=MAX(INT((VUPPER-VLOWER)/VINCR+0.5)+1,1)
38 | C DO 100 ICALC=1,NCALCS
39 | C VARVAL=VLOWER+VINCR*(ICALC-1)
40 | C
41 | C SET NEXT VALUE OF VARIABLE TO BE INCREMENTED
42 | C
43 | C IF (IVAR.EQ.1) THEN
44 | C XWALL=VARVAL
45 | C ELSE IF (IVAR.EQ.2) THEN
46 | C YWALL=VARVAL
47 | C ELSE IF (IVAR.EQ.3) THEN
48 | C T(0)=VARVAL
49 | C ELSE IF (IVAR.EQ.4) THEN
50 | C L(ISUB)=VARVAL
51 | C IF (ISUB.EQ.1) ZSTOVE=VARVAL
52 | C ELSE IF (IVAR.EQ.5) THEN
53 | C WIDTH(ISUB)=VARVAL
54 | C IF (ISUB.EQ.0) WSTOVE=VARVAL
55 | C XSTOVE=WSTRVE/2.
56 | C ELSE IF (IVAR.EQ.6) THEN
57 | C HEIGHT(ISUB)=VARVAL
58 | C IF (ISUB.EQ.0) HSTOVE=VARVAL
59 | C ELSE IF (IVAR.EQ.7) THEN
60 | C K(ISUB)=VARVAL
61 | C ELSE IF (IVAR.EQ.8) THEN
62 | C EMMIS(ISUB)=VARVAL
63 | C END IF
64 | C
65 | C INITIALIZE THE COUNTERS TO ZERO
66 | C
67 | C ITER=0
68 | C
69 | C INITIALIZE TEMPERATURE GUESSES TO WORST CASE CONDITIONS
70 | C

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71      DO 20 I=1,N-1
72      20  T(I)=T(N)
73          TDIFF=T(0)-T(N)
74          TGOAL=T(N)
75      C
76      C DETERMINE NEXT GUESS FOR TEMPERATURES
77      C
78          DO 30 I=1,N-1
79      30  T(I)=T(I)+TDIFF/N
80      C
81      C CALCULATE TOTAL RESISTANCE AND HEAT FLOW FROM GUESSED TEMPERATURES
82      C
83          CALL HEATS
84      40  INNER=0
85      C
86      C CALCULATE WITH NEWLY GUESSED TEMPERATURES AND HEATS
87      C
88          DO 60 I=1,N
89          TINC=ABS(TDIFF/N/TSTEP1)
90          TINCI=TINC
91          QSIGN=DSIGN(1.D0,Q(I)-QTOTAL)
92      C
93      C GO THROUGH INNER ITERATION LOOP AT LEAST ONCE FOR SOME FORCED
94      C IMPROVEMENT
95      C
96          THRU1=.FALSE.
97      50  IF (.NOT. (ABS((Q(I)-QTOTAL)/QTOTAL).LE.QEPS.AND.THRU1)) THEN
98          INNER=INNER+1
99          THRU1=.TRUE.
100         IF (ABS((Q(I)-QTOTAL)/QTOTAL).GT.QEPS) NOTYET=.TRUE.
101         IF (MATL(I).NE.'AIRSPACE') THEN
102      C
103      C HEAT TRANSFER IS CONDUCTION, CALCULATE TEMPERATURE
104      C
105         T(I)=T(I-1)-QTOTAL*R(I)
106         ELSE
107      C
108      C HEAT TRANSFER IS BY CONVECTION & RADIATION, SEARCH FOR TEMPERATURE
109      C
110         T(I)=T(I)+QSIGN*TINC
111      C
112      C RECALCULATE THE HEAT FLOW AND COMPARE TO TOTAL HEAT
113      C
114         CALL HEAT(I)
115         IF (DSIGN(1.D0,Q(I)-QTOTAL).NE.QSIGN) THEN
116             TINCI=TINCI/TSTEP2
117             TINC=TINCI
118             QSIGN=DSIGN(1.D0,Q(I)-QTOTAL)
119         ELSE
120             TINC=TINC*2.
121         END IF
122         GO TO 50
123     END IF
124 END IF
125 C
126 C RECALCULATE TOTAL HEAT WITH THE NEW TEMPERATURES AND PROCEED
127 C
128     CALL HEATS
129      60  CONTINUE
130 C
131 C IF DEBUG IS ON, PRINT OUT A SUMMARY OF THE ITERATION
132 C
133     ITER=ITER+1
134     IF (DEBUG.AND.NOTYET) THEN
135         WRITE (6,7) ITER,INNER
136         WRITE (6,'(1X,A,F7.2)') 'STOVE TEMPERATURE: ',T(0)-273.15
137         WRITE (6,'(1X,A,F8.2,A,F8.3)') 'TOTAL HEAT: ',QTOTAL,
138             ' TOTAL RESISTANCE: ',RTOTAL
139     WRITE (6,3)
140     DO 70 I=1,N

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141 IF (MATL(I).EQ.'AIRSPACE'.AND.I.EQ.1) THEN
142 WRITE (6,5) MATL(I),T(I)-273.15,R(I),Q(I),CF(I)
143 ELSE IF (MATL(I).EQ.'AIRSPACE'.AND.I.NE.1) THEN
144 WRITE (6,1) MATL(I),T(I)-273.15,R(I),Q(I),H(I),CF(I)
145 ELSE
146 WRITE (6,2) MATL(I),T(I)-273.15,R(I),Q(I)
147 END IF
148 70 CONTINUE
149 TDIFF=T(N)-TGOAL
150 WRITE (6,'(1X,A7,F10.3,A)') 'TDIFF: ',TDIFF,
151 2 CMET(TDIFF/TGOAL,EPS)
152 WRITE (6,6) 'QMET: ',(Q(I)-QTOTAL,
153 2 CMET((Q(I)-QTOTAL)/QTOTAL,EPS),I=1,N)
154 END IF
155 TDIFF=T(N)-TGOAL
156 T(N)=TGOAL
157 C
158 C IF ANY OF THE INDIVIDUAL HEATS HAVEN'T CONVERGED ON THE FINAL VALUE,
159 C CONTINUE WITH THE PROCESS UNTIL ALL ARE EQUAL
160 C
161 NOTYET=.FALSE.
162 DO 80 I=1,N
163 IF (ABS((Q(I)-QTOTAL)/QTOTAL).GT.EPS) NOTYET=.TRUE.
164 80 CONTINUE
165 IF (ABS(TDIFF)/TGOAL.GT.EPS) NOTYET=.TRUE.
166 IF (NOTYET) GO TO 40
167 C
168 C THE SOLUTION HAS BEEN FOUND, PRINT IT OUT
169 C
170 IF (.NOT.FULPRT) THEN
171 WRITE (6,9) VARVAL,(T(I)-273.15,I=0,N)
172 ELSE
173 WRITE (6,4) TITLE
174 WRITE (6,'(1X,A,I3)') 'ITERATIONS: ',ITER
175 WRITE (6,'(1X,3A,F8.3)') 'VARIED VARIABLE: ',VNAME,' = ',
176 2 VARVAL
177 WRITE (6,'(1X,A,F7.2)') 'STOVE TEMPERATURE: ',T(0)-273.15
178 WRITE (6,'(1X,A,F8.2,A,F8.3)') 'TOTAL HEAT: ',QTOTAL,
179 2 ' TOTAL RESISTANCE: ',RTOTAL
180 WRITE (6,3)
181 DO 90 I=1,N
182 IF (MATL(I).EQ.'AIRSPACE'.AND.I.EQ.1) THEN
183 WRITE (6,5) MATL(I),T(I)-273.15,R(I),Q(I),Q(I)
184 ELSE IF (MATL(I).EQ.'AIRSPACE'.AND.I.NE.1) THEN
185 QCONV=(T(I-1)-T(I))/CONV(I)
186 QRAD=(T(I-1)-T(I))/RAD(I)
187 WRITE (6,1) MATL(I),T(I)-273.15,R(I),Q(I),QCONV,QRAD
188 ELSE
189 WRITE (6,2) MATL(I),T(I)-273.15,R(I),Q(I)
190 END IF
191 90 CONTINUE
192 WRITE (6,4) 'TEMPERATURES ARE OF COOLER SIDE OF NODE'
193 END IF
194 100 CONTINUE
195 GO TO 10
196 END IF
197 STOP
198 1 FORMAT (1X,A10,2X,F10.2,3X,F10.3,2X,F10.3,3X,F10.3,3X,F10.3)
199 2 FORMAT (1X,A10,2X,F10.2,3X,F10.3,2X,F10.3)
200 3 FORMAT ('0 MATERIAL TEMPERATURE RESISTANCE HEAT CONV
201 2ECTION RADIATION',/)
202 4 FORMAT ('0',A)
203 5 FORMAT (1X,A10,2X,F10.2,3X,F10.3,2X,F10.3,16X,F10.3)
204 6 FORMAT (1X,A7,4(F10.3,A5,:),/,10(8X,4(F10.3,A5,:),/))
205 7 FORMAT ('0 ITERATION: ',I3,' INNER LOOP: ',I3)
206 8 FORMAT (' ',A10,20(A7,:))
207 9 FORMAT (' ',F10.3,20(F6.1,1X,:))
208 11 FORMAT ('0',/,20(' ',I6,' : ',A,/))
209 12 FORMAT (' ',A10,20(' (' ,I2,' )',:))
210 END

```

211		SUBROUTINE INPUT (THEEND)		1
212	C			2
213	C	#####		3
214	C	#####		4
215	C	#####		5
216	C	#####		6
217	C	#####		7
218	C	#####		8
219	C	#####		9
220	C	#####		10
221	C			11
222	C	PURPOSE: INPUTS DATA DESCRIBING THE STOVE / WALL PROTECTION SYSTEM		12
223	C	TO BE MODELED		13
224	C			14
225		INCLUDE 'STOVE.CMN'		15
226		PARAMETER (NVAR=8)		16
227		CHARACTER VAR(NVAR)*6,IN*80,KEYWD*80		17
228		INTEGER VLEN(NVAR)		18
229		LOGICAL THEEND,HAVEY,HAVEY		19
230		DATA (VAR(I),VLEN(I),I=1,NVAR) /'XWALL ',5,'YWALL ',5,'TSTOVE',6,		20
231		2 'THICK ',5,'WIDTH ',5,'HEIGHT ',6,'K ',1,'EMMIS ',5/		21
232	C			22
233	C	LOOK FOR A KEYWORD OR END OF FILE		23
234	C			24
235		THEEND=.TRUE.		25
236		HAVEY=.FALSE.		26
237		HAVEY=.FALSE.		27
238		TITLE='STOVE / WALL PROTECTOR HEAT TRANSFER MODEL'		28
239		N=0		29
240		IVAR=0		30
241		VNAME=' '		31
242	10	READ (5,'(A80)',END=30) IN		32
243		THEEND=.FALSE.		33
244		IS=INDEX(IN,':')		34
245		IF (IS.GT.1) THEN		35
246		KEYWD=IN(1:IS-1)		36
247		IF (KEYWD.NE.'END') THEN		37
248	C			38
249	C	XWALL ... X POSITION OF POINT ON THE WALL		39
250	C			40
251		IF (KEYWD.EQ.'XWALL') THEN		41
252		ICHR=IS+2		42
253		XWALL=FVAL(IN,ICHR)		43
254		HAVEY=.TRUE.		44
255	C			45
256	C	YWALL ... Y POSITION OF POINT ON THE WALL		46
257	C			47
258		ELSE IF (KEYWD.EQ.'YWALL') THEN		48
259		ICHR=IS+2		49
260		YWALL=FVAL(IN,ICHR)		50
261		HAVEY=.TRUE.		51
262	C			52
263	C	AIRSPACE ... AN AIR SPACE BETWEEN TWO SOLID PROTECTORS		53
264	C			54
265		ELSE IF (KEYWD.EQ.'AIRSPACE') THEN		55
266		N=N+1		56
267		MATL(N)='AIRSPACE'		57
268		ICHR=IS+2		58
269		V1=FVAL(IN,ICHR)		59
270		V2=FVAL(IN,ICHR)		60
271		V3=FVAL(IN,ICHR)		61
272		IF (V2.EQ.0..AND.V3.EQ.0.) THEN		62
273		T(N)=V1		63
274		EMMIS(N)=1.0		64
275		HEIGHT(N)=0.		65
276		ELSE		66
277		L(N)=V1		67
278		EMMIS(N)=V2		68
279		IF (EMMIS(N).EQ.0.) EMMIS(N)=1.0		69
280		T(N)=V3		70

281		HEIGHT(N)=HEIGHT(N-1)	71
282		WIDTH(N)=WIDTH(N-1)	72
283		END IF	73
284	C		74
285	C	STOVE ... THE HOT STOVE SURFACE	75
286	C		76
287		ELSE IF (KEYWD.EQ.'STOVE') THEN	77
288		MATL(0)='STOVE'	78
289		ICHR=IS+2	79
290		EMMIS(0)=FVAL(IN,ICHR)	80
291		IF (EMMIS(0).EQ.0.) EMMIS(N)=1.0	81
292		HEIGHT(0)=FVAL(IN,ICHR)	82
293		WIDTH(0)=FVAL(IN,ICHR)	83
294		T(0)=FVAL(IN,ICHR)	84
295	C		85
296	C	FOR ... SPECIFIES A SERIES OF CALCULATIONS TO BE DONE	86
297	C		87
298		ELSE IF (KEYWD.EQ.'FOR') THEN	88
299		IVAR=0	89
300		ISUB=0	90
301		DO 20 I=1,NVAR	91
302		J=INDEX(IN,VAR(I)(1:VLEN(I)))	92
303		IF (J.NE.0.AND.IN(J-1:J-1).EQ.' ') IVAR=I	93
304	20	CONTINUE	94
305		IR=0	95
306		ICHR=IS+2	96
307		IF (IVAR.EQ.0) THEN	97
308		WRITE (6,1) IN	98
309		GO TO 10	99
310	C		100
311	C	IF IT'S A VARIABLE WITH SUBSCRIPT, MAKE SURE ONE'S THERE	101
312	C		102
313		ELSE IF (IVAR.GE.4) THEN	103
314		IL=INDEX(IN,'(')	104
315		IR=INDEX(IN,')')	105
316		IF (IL.EQ.0.OR.IR.EQ.0.OR.IL.GT.IR) THEN	106
317		WRITE (6,2) IN	107
318		GO TO 10	108
319		END IF	109
320		ISUB=FVAL(IN,ICHR)	110
321		END IF	111
322		ICHR=IR+1	112
323		VLOWER=FVAL(IN,ICHR)	113
324		VUPPER=FVAL(IN,ICHR)	114
325		VINCR=FVAL(IN,ICHR)	115
326		IF ((VLOWER.NE.VUPPER.AND.VINCR.EQ.0)	116
327	2	.OR.(VLOWER.EQ.VUPPER.AND.VINCR.NE.0)	117
328	3	.OR.(VUPPER.GT.VLOWER.AND.VINCR.LT.0)	118
329	4	.OR.(VUPPER.LT.VLOWER.AND.VINCR.GT.0)) THEN	119
330		WRITE (6,4) IN	120
331		GO TO 10	121
332		END IF	122
333		VNAME=VAR(IVAR)	123
334		VNAME(VLEN(IVAR)+1:VLEN(IVAR)+1+IR-IL)=IN(IL:IR)	124
335	C		125
336	C	DEBUG ... TURN DEBUG PRINT ON OR OFF	126
337	C		127
338		ELSE IF (KEYWD.EQ.'DEBUG') THEN	128
339		IF (INDEX(IN,'OFF').NE.0) DEBUG=.FALSE.	129
340		IF (INDEX(IN,'ON').NE.0) DEBUG=.TRUE.	130
341	C		131
342	C	PRINTOUT ... SPECIFY LEVEL OF PRINTOUT	132
343	C		133
344		ELSE IF (KEYWD.EQ.'PRINTOUT') THEN	134
345		IF (INDEX(IN,'FULL').NE.0) FULPRT=.TRUE.	135
346		IF (INDEX(IN,'FULL').EQ.0) FULPRT=.FALSE.	136
347	C		137
348	C	TITLE ... SPECIFY A TITLE FOR THE PRINTOUT	138
349	C		139
350		ELSE IF (KEYWD.EQ.'TITLE') THEN	140

351		TITLE=IN(IS+2:80)	141
352	C		142
353	C	IF IT'S NOT ONE OF THE RECOGNIZED KEYWORDS, ASSUME A SOLID PROTECTOR	143
354	C		144
355		ELSE	145
356		N=N+1	146
357		ICHR=IS+2	147
358		MATL(N)=IN(1:IS-1)	148
359		L(N)=FVAL(IN,ICHR)	149
360		HEIGHT(N)=FVAL(IN,ICHR)	150
361		WIDTH(N)=FVAL(IN,ICHR)	151
362		K(N)=FVAL(IN,ICHR)	152
363		EMMIS(N)=FVAL(IN,ICHR)	153
364		T(N)=FVAL(IN,ICHR)	154
365		IF (L(N).EQ.0..OR.HEIGHT(N).EQ.0..OR.WIDTH(N).EQ.0..OR.	155
366	2	K(N).EQ.0..OR.EMMIS(N).EQ.0.) THEN	156
367		WRITE (6,3) IN	157
368		N=N-1	158
369		GO TO 10	159
370		END IF	160
371		END IF	161
372		GO TO 10	162
373		END IF	163
374		END IF	164
375	C		165
376	C	DATA HAS BEEN READ IN, CHECK CONSISTENCY OF DATA INPUT	166
377	C		167
378	30	IF (THEEND) THEN	168
379		RETURN	169
380		ELSE IF (N.LE.1) THEN	170
381		WRITE (6,*) 'DATA INPUT ERROR, TOO FEW NODES SPECIFIED.'	171
382		ELSE	172
383		IF (DEBUG.AND.IVAR.NE.0) THEN	173
384		IF (IVAR.LT.4) THEN	174
385		WRITE (6,5) VAR(IVAR),VLOWER,VUPPER,VINCR	175
386		ELSE	176
387		WRITE (6,6) VAR(IVAR),ISUB,VLOWER,VUPPER,VINCR	177
388		END IF	178
389		END IF	179
390		DO 40 I=1,N	180
391		IF (DEBUG) CALL PSUM(I)	181
392		IF (MATL(I).EQ.'AIRSPACE') THEN	182
393		IF ((L(I).LE.0..AND.I.NE.N).OR.(HEIGHT(I).LE.0..AND.I.NE.N)	183
394	2	.OR.(HEIGHT(I).NE.0..AND.I.EQ.N).OR.EMMIS(I).LE.0.) THEN	184
395		WRITE (6,'(1X,A,I3)') 'INCORRECTLY SPECIFIED AIR SPACE.',I	185
396		STOP 'INPUT DATA ERRORS, AIR SPACE'	186
397		END IF	187
398		ELSE	188
399		IF (L(I).LE.0..OR.HEIGHT(I).LE.0..OR.WIDTH(I).LE.0..OR.	189
400	2	K(I).LE.0..OR.EMMIS(I).LE.0.) THEN	190
401		WRITE (6,'(1X,A,I3)') 'INCORRECTLY SPECIFIED PROTECTOR.',I	191
402		STOP 'INPUT DATA ERRORS, SOLID PROTECTOR'	192
403		END IF	193
404		END IF	194
405	40	CONTINUE	195
406		IF (XWALL.LT.0..OR.YWALL.LT.0.) THEN	196
407		WRITE (6,*) 'INCORRECTLY SPECIFIED POINT ON WALL.'	197
408		STOP 'DATA INPUT ERRORS, XWALL & YWALL'	198
409		END IF	199
410		IF (T(0).LE.T(N)) THEN	200
411		WRITE (6,*) 'INCORRECTLY SPECIFIED ENDPOINT TEMPERATURES.'	201
412		STOP 'DATA INPUT ERRORS, T(0) & T(N)'	202
413		END IF	203
414		IF (T(0).LE.0..OR.WIDTH(0).LE.0..OR.HEIGHT(0).LE.0..OR.EMMIS(0)	204
415	2	.LE.0.) THEN	205
416		WRITE (6,*) 'INCORRECTLY SPECIFIED STOVE PARAMETERS.'	206
417		STOP 'DATA INPUT ERRORS, STOVE'	207
418		END IF	208
419		END IF	209
420		IF (MATL(N).EQ.'AIRSPACE') HEIGHT(N)=HEIGHT(N-1)	210

421		ZSTOVE=L(1)		211
422		HSTOVE=HEIGHT(0)		212
423		WSTOVE=WIDTH(0)		213
424	C			214
425	C	IF NOT POSITION HAS BEEN SPECIFIED, USE MIDPOINT OF STOVE		215
426	C			216
427		IF (.NOT. HAVEX) THEN		217
428		XWALL=WSTOVE/2.		218
429		END IF		219
430		IF (.NOT. HAVEY) THEN		220
431		YWALL=HSTOVE/2.		221
432		END IF		222
433	C			223
434	C	IF NO INCREMENT HAS BEEN SPECIFIED, MAKE ONE UP		224
435	C			225
436		IF (IVAR.EQ.0) THEN		226
437		IVAR=1		227
438		VLOWER=XWALL		228
439		VUPPER=XWALL		229
440		VINCR=1.0		230
441		END IF		231
442	C			232
443	C	PRINT OUT A DESCRIPTION OF THE STOVE / WALL SYSTEM AS SPECIFIED		233
444	C			234
445		WRITE (6,11) TITLE,N+1,XWALL,YWALL		235
446		IF (IVAR.GT.0.AND.IVAR.LT.4) THEN		236
447		WRITE (6,5) VAR(IVAR),VLOWER,VUPPER,VINCR		237
448		ELSE IF (IVAR.GT.4) THEN		238
449		WRITE (6,6) VAR(IVAR),ISUB,VLOWER,VUPPER,VINCR		239
450		END IF		240
451		WRITE (6,12)		241
452		DO 50 I=0,N		242
453		IF (I.EQ.0.OR.I.EQ.N) THEN		243
454		IF (MATL(I).EQ.'STOVE') THEN		244
455		WRITE (6,13) I,MATL(I),HEIGHT(I),WIDTH(I),EMMIS(I),T(I)-273.15		245
456		ELSE IF (MATL(I).EQ.'AIRSPACE') THEN		246
457		WRITE (6,14) I,MATL(I),L(I),EMMIS(I),T(I)-273.15		247
458		ELSE		248
459		WRITE (6,15) I,MATL(I),HEIGHT(I),WIDTH(I),L(I),EMMIS(I),K(I),		249
460		2 T(I)-273.15		250
461		END IF		251
462		ELSE		252
463		IF (MATL(I).EQ.'STOVE') THEN		253
464		WRITE (6,13) I,MATL(I),HEIGHT(I),WIDTH(I),EMMIS(I)		254
465		ELSE IF (MATL(I).EQ.'AIRSPACE') THEN		255
466		WRITE (6,14) I,MATL(I),L(I),EMMIS(I)		256
467		ELSE		257
468		WRITE (6,15) I,MATL(I),HEIGHT(I),WIDTH(I),L(I),EMMIS(I),K(I)		258
469		END IF		259
470		END IF		260
471	50	CONTINUE		261
472		RETURN		262
473	C			263
474	1	FORMAT ('OSYNTAX ERROR ON ''FOR'' STATEMENT, ILLEGAL OR NO VARIABLE		264
475		2E SPECIFIED.',/,',',A79,//)		265
476	2	FORMAT ('OSYNTAX ERROR ON ''FOR'' STATEMENT, SUBSCRIPT REQUIRED FOR		266
477		2R VARIABLE SPECIFIED.',/,',',A79,//)		267
478	3	FORMAT ('OSYNTAX ERROR ON STATEMENT, UNRECOGNIZED KEYWORD.',/,		268
479		2 ' ',A79,//)		269
480	4	FORMAT ('OSYNTAX ERROR ON ''FOR'' STATEMENT, RANGE AND INCREMENT IN		270
481		2NCONSISTENT.',/,',',A79,//)		271
482	5	FORMAT ('OSERIES OF CALCULATIONS FOR VARIABLE ',A,': ',3F10.3)		272
483	6	FORMAT ('OSERIES OF CALCULATIONS FOR VARIABLE ',A,','(',I2,		273
484		2 ' '): ',3F10.3)		274
485	11	FORMAT ('1',A,//,		275
486		2 ' NUMBER OF NODES IN CALCULATION: ',I2,/, ' POINT ON WALL: (X):',		276
487		3 F10.3,T41, '(Y):',F10.3)		277
488	12	FORMAT ('OI MATERIAL HEIGHT WIDTH THICK EMISS		278
489		2 K TEMPERATURE',/,		279
490		3 ' (m) (m) (m)		280

491		4	(W/m K)	(°C)',/, ' ',78('—'),/)		281
492	13	FORMAT	(1X,I2,2X,A,T26,1X,F6.2,T35,F6.2,T51,F6.2,T70,F7.2)		282	
493	14	FORMAT	(1X,I2,2X,A,T43,F6.2,T51,F6.2,T70,F7.2)		283	
494	15	FORMAT	(1X,I2,2X,A,T26,1X,4(F6.2,2X),F8.3,2X,F8.2)		284	
495		END			285	

496		DOUBLE PRECISION FUNCTION FVAL (IN,ICHR)		1
497	C			2
498	C	#####		3
499	C	#####		4
500	C	#####		5
501	C	#####		6
502	C	#####		7
503	C	#####		8
504	C	#####		9
505	C			10
506	C	ARGUMENTS: IN: STRING CONTAINING (MAYBE) NUMBER		11
507	C	ICHR: (INPUT) BEGINNING CHARACTER POSITION		12
508	C	(OUTPUT) NEXT CHARACTER POSITION		13
509	C			14
510	C	PURPOSE: DECODE NEXT NUMBER IN STRING AS A DOUBLE PRECISION VALUE		15
511	C			16
512		IMPLICIT DOUBLE PRECISION (A-H,O-Z)		17
513		CHARACTER IN*(*),FORMAT*10		18
514		IL=LEN(IN)		19
515		IFIRST=ICHR		20
516		DO 20 I=IFIRST,IL		21
517		IF ((IN(I:I).GE.'0'.AND.IN(I:I).LE.'9').OR.IN(I:I).EQ.'.'		22
518		2 .OR.IN(I:I).EQ.'+'.OR.IN(I:I).EQ.'-') THEN		23
519	C			24
520	C	THERE IS A NUMBER ON THE CARD, FIND OUT WHAT IT IS		25
521	C			26
522		DO 10 J=I,IL		27
523	C			28
524	C	IF WE FIND THE END OF THE NUMBER, READ IT FROM THE LINE		29
525	C			30
526		IF ((IN(J:J).LT.'0'.OR.IN(J:J).GT.'9').AND.IN(J:J).NE.'.'		31
527		2 .AND.IN(J:J).NE.'+'.AND.IN(J:J).NE.'-') THEN		32
528		WRITE (FORMAT,30) J-I		33
529		READ (IN(I:J-1),FORMAT) VAL		34
530		FVAL=VAL		35
531		ICHR=J		36
532		RETURN		37
533		END IF		38
534	10	CONTINUE		39
535	C			40
536	C	IF WE GET TO THE END OF THE LINE WITHOUT FINDING END OF NUMBER,		41
537	C	JUST READ THE NUMBER		42
538	C			43
539		WRITE (FORMAT,30) IL-I+1		44
540		READ (IN(I:IL),FORMAT) VAL		45
541		FVAL=VAL		46
542		ICHR=J		47
543		RETURN		48
544		END IF		49
545	20	CONTINUE		50
546	C			51
547	C	IF NO NUMBER IS ON THE CARD, JUST RETURN A 0.		52
548	C			53
549		FVAL=0.		54
550		RETURN		55
551	C			56
552	30	FORMAT ('(F',I2.2,'.0)')		57
553		END		58

554		SUBROUTINE HEATS		1
555				2
556	C			3
557	C	0000 0		4
558	C	0000 0 000000 000000 000000 000000		5
559	C	00000000 0 000 0 0000 000		6
560	C	0000 0 000000 000000 0000 000000		7
561	C	0000 0 0 0 000 0000 000		8
562	C	0000 0 000000 000000 0000 000000		9
563	C			10
564	C	ARGUMENTS: NONE		11
565	C			12
566	C	PURPOSE: CALCULATES TOTAL HEAT AND TOTAL RESISTANCE THROUGH WALL		13
567	C	PROTECTORS		14
568	C			15
569		INCLUDE 'STOVE.CMN'		16
570	C			17
571	C	JUST SUM UP RESISTANCES TO MAKE UP TOTAL RESISTANCE		18
572	C			19
573		RTOTAL=0.		20
574		DO 10 I=1,N		21
575		CALL HEAT(I)		22
576	10	RTOTAL=RTOTAL+R(I)		23
577	C			24
578	C	TOTAL HEAT IS JUST DELTA T / TOTAL RESISTANCE		25
579	C			26
580		QTOTAL=(T(0)-T(N))/RTOTAL		27
581		RETURN		28
582		END		29

644		DOUBLE PRECISION FUNCTION CFIGS (A,B,C)		1
645	C			2
646	C	00000000 0000 0000		3
647	C	0 0000 0 0		4
648	C	0 0000 000000 0000 000000 000000		5
649	C	0 0000 0000 0000 000000 000		6
650	C	0 0000 0000 0000 0 000000		7
651	C	0 0000 0000 0000 00000000 000		8
652	C	00000000 0000 0000 0 0000 000000		9
653	C			10
654	C			11
655	C	ARGUMENTS: A: WIDTH OF RECTANGLE		12
656	C	B: HEIGHT OF RECTANGLE		13
657	C	C: DISTANCE TO POINT OF CALCULATION		14
658	C			15
659	C	PURPOSE: CALCULATES RADIATION CONFIGURATION FACTOR FOR A PLANE		16
660	C	ELEMENT TO A PLANE PARALLEL RECTANGLE.		17
661	C			18
662	C	SOURCE: THERMAL RADIATION HEAT TRANSFER, SEIGEL & HOWELL.		19
663	C			20
664		IMPLICIT DOUBLE PRECISION (A-H,O-Z)		21
665		PI=3.14159		22
666		X=A/C		23
667		Y=B/C		24
668		CFIGS=1. / (2*PI)*(X/SQRT(1+X**2)*ATAN(Y/SQRT(1+X**2))		25
669		2 + Y/SQRT(1+Y**2)*ATAN(X/SQRT(1+Y**2)))		26
670		RETURN		27
671		END		28

672		DOUBLE PRECISION FUNCTION CFIGP (A,B,C)		1
673	C			2
674	C	00000000 0000 0000		3
675	C	0 0000 0 0		4
676	C	0 0000 000000 0000 000000 000000		5
677	C	0 0000 0000 0000 000000 000 0		6
678	C	0 0000 0000 0000 0 000 0		7
679	C	0 0000 0000 0000 00000000 000000		8
680	C	00000000 0000 0000 0 0000 000		9
681	C			10
682	C			11
683	C	ARGUMENTS: A: WIDTH OF RECTANGLE		12
684	C	B: HEIGHT OF RECTANGLE		13
685	C	C: DISTANCE BETWEEN RECTANGLES		14
686	C			15
687	C	PURPOSE: CALCULATES RADIATION CONFIGURATION FACTOR FOR TWO		16
688	C	IDENTICAL, PARALLEL, DIRECTLY OPPOSED RECTANGLES.		17
689	C			18
690	C	SOURCE: THERMAL RADIATION HEAT TRANSFER, SEIGEL & HOWELL.		19
691	C			20
692		IMPLICIT DOUBLE PRECISION (A-H,O-Z)		21
693		PI=3.14159		22
694		X=A/C		23
695		Y=B/C		24
696		CFIGP=2./ (PI*X*Y)*(LOG(((1+X*X)*(1+Y*Y))/(1+X*X+Y*Y))**0.5 +		25
697		2 X*SQRT(1+Y*Y)*ATAN(X/SQRT(1+Y*Y)) +		26
698		3 Y*SQRT(1+X*X)*ATAN(Y/SQRT(1+X*X)) -		27
699		4 X*ATAN(X) - Y*ATAN(Y))		28
700		RETURN		29
701		END		30

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702 |      DOUBLE PRECISION FUNCTION HCONV(T1,T2,L)      |      1
703 | C                                                  |      2
704 | C      @@@@ @                                     |      3
705 | C      @@@@ @                                     |      4
706 | C      @@@@ @ @@@@@ @@@@@ @@@@@ @@@ @          |      5
707 | C      @@@@@@@ @ @@@ @@@ @ @ @@@ @@@ @        |      6
708 | C      @@@@ @ @ @@@ @@@ @ @ @@@ @@@ @        |      7
709 | C      @@@@ @ @ @@@ @@@ @ @ @@@ @@@@         |      8
710 | C      @@@@ @ @@@@@ @@@@@ @ @@@ @@           |      9
711 | C                                                  |     10
712 | C  ARGUMENTS:   T1:  TEMPERATURE OF HOTTER SURFACE |     11
713 | C               T2:  TEMPERATURE OF COOLER SURFACE |     12
714 | C               L:   HEIGHT OF SURFACES             |     13
715 | C                                                  |     14
716 | C  PURPOSE:  CALCULATES FREE CONVECTION HEAT TRANSFER COEFFICIENT FOR |     15
717 | C             A VERTICAL SURFACE.                  |     16
718 | C                                                  |     17
719 | C  SOURCE:  FUNDAMENTALS OF HEAT TRANSFER, INCORPERA & DEWITT. |     18
720 | C                                                  |     19
721 | C      IMPLICIT DOUBLE PRECISION (A-H,O-Z)          |     20
722 | C      DOUBLE PRECISION K,NU,L,NUSELT              |     21
723 | C      DIMENSION C(3,5)                            |     22
724 | C      DATA ((C(I,J),J=1,5),I=1,3) /             |     23
725 | C      2 -.381021E-2, .132063E-3, -.117332E-6, .687499E-10, -.127680E-13 |     24
726 | C      3,-.167333E-4, .143076E-6, -.249135E-10, .781850E-13, -.127693E-16 |     25
727 | C      4,-.501195E-5, .468550E-7, .881329E-10,-.117315E-13, .307192E-17 |     26
728 | C      5 /                                           |     27
729 | C      TF=(T1+T2)/2                                |     28
730 | C      DELTAT=(T1-T2)                              |     29
731 | C      K=C(1,1)+C(1,2)*TF+C(1,3)*TF*TF+C(1,4)*TF**3+C(1,5)*TF**4      |     30
732 | C      ALPHA=C(2,1)+C(2,2)*TF+C(2,3)*TF*TF+C(2,4)*TF**3+C(2,5)*TF**4    |     31
733 | C      NU=C(3,1)+C(3,2)*TF+C(3,3)*TF*TF+C(3,4)*TF**3+C(3,5)*TF**4      |     32
734 | C      PR=NU/ALPHA                                  |     33
735 | C      RA=9.8*(1./TF)*ABS(DELTAT)*L**3/(NU*ALPHA)   |     34
736 | C      NUSELT=(0.825+0.387*RA**(1./6.))/(1.+(0.492/PR)**(9./16.))      |     35
737 | C      2 ** (8./27.))**2                            |     36
738 | C      HCONV=NUSELT*K/L                             |     37
739 | C      RETURN                                        |     38
740 | C      END                                           |     39

```

741		CHARACTER*5 FUNCTION CMET(VALUE,EPS)		1
742	C			2
743	C	CCCCCCCC		3
744	C	C CCCC		4
745	C	C CCCC CCCCCC CCCCCC CCCCCC		5
746	C	C C CCCC C CCCC C CCCC CCCCC		6
747	C	C CCCC C CCCC CCCCCC CCCCC		7
748	C	C CCCC C CCCC C CCCCC CCCCC		8
749	C	CCCCCCCC C CCCC CCCCCC CCCCC		9
750	C			10
751	C	ARGUMENTS: VALUE: NUMBER TO BE EVALUATED		11
752	C	EPS: ACCEPTANCE CRITERION FOR VALUE		12
753	C			13
754	C	PURPOSE: FUNCTIONS RETURNS A CHARACTER INDICATION OF WHETHER THE		14
755	C	VALUE IS WITHIN LIMITS. USED FOR DEBUG PRINTOUT		15
756	C			16
757		IMPLICIT DOUBLE PRECISION (A-H,O-Z)		17
758		IF (ABS(VALUE).LE.EPS) THEN		18
759		CMET='(IN) '		19
760		ELSE		20
761		CMET='(OUT)'		21
762		END IF		22
763		RETURN		23
764		END		24

765	SUBROUTINE PSUM(I)	1
766	C	2
767	C 00000000	3
768	C 0000 0	4
769	C 0000 0 000000 000 0 0000000	5
770	C 00000000 000 000 0 0 0 000	6
771	C 0000 000000 000 0 0 0 000	7
772	C 0000 000 000 0 0 0 000	8
773	C 0000 000000 000000 0 0 000	9
774	C	10
775	C ARGUMENTS: I: SURFACE NUMBER FOR SUMMARY PRINTOUT	11
776	C	12
777	C PURPOSE: PRINTS OUT ALL THE VARIABLES IN THE COMMON BLOCK. USED	13
778	C FOR DEBUG PRINTOUT.	14
779	C	15
780	C INCLUDE 'STOVE.COM'	16
781	C WRITE (6,10) I,MAIL(I),T(I),R(I),L(I),K(I),E(I),CF(I),EMIS(I),	17
782	C 2 Q(I),CONV(I),RAD(I),HEIGHT(I),WIDTH(I),XSTOVE,YSTOVE,ZSTOVE,	18
783	C 3 WSTOVE,ESTOVE,YWALL,YWALL,RTOTAL,QTOTAL,N	19
784	C RETURN	20
785	C	21
786	10 FORMAT ('CURRENT VALUES FOR SPACE ',I2,' MATERIAL IS ',A,/,	22
787	2 ' TEMPERATURE:',F10.3,T41,'RESISTANCE:',F10.3,/,	23
788	3 ' THICKNESS:',F10.3,T41,'THERMAL CONDUCTIVITY:',E12.5,/,	24
789	4 ' E:',F10.3,T41,'CONFIGURATION FACTOR:',F10.3,/,	25
790	5 ' EMISSIVITY:',F10.3,T41,'INDIVIDUAL HEAT:',F10.3,/,	26
791	6 ' CONV. RESISTANCE:',F10.3,T41,'RAD. RESISTANCE:',F10.3,/,	27
792	7 ' HEIGHT:',F10.3,T41,'WIDTH:',F10.3,/,	28
793	8 ' XSTOVE:',F10.3,T31,'YSTOVE:',F10.3,T61,'ZSTOVE:',F10.3,/,	29
794	9 ' WSTOVE:',F10.3,T31,'ESTOVE:',F10.3,/,	30
795	* ' YWALL: ',F10.3,T31,'YWALL: ',F10.3,/,	31
796	1 ' RTOTAL:',F10.3,T31,'QTOTAL:',F10.3,T61,'N: ',I10)	32
797	END	33

	C	COMMON BLOCK FOR PROGRAM STOVE	
	C		
1		IMPLICIT DOUBLE PRECISION (A-H,O-Z)	1
2	C		2
3		PARAMETER (MAXPRO=20)	3
4	C		4
5		DOUBLE PRECISION L,K	5
6		CHARACTER MATL*40,VNAME*10,TITLE*80	6
7		LOGICAL DEBUG,FULPRT	7
8		COMMON /NSTOVE/ T(0:MAXPRO),R(0:MAXPRO),L(0:MAXPRO),K(0:MAXPRO),	8
9		2 H(0:MAXPRO),CF(0:MAXPRO),EMMIS(0:MAXPRO),Q(0:MAXPRO),	9
10		3 CONV(0:MAXPRO),RAD(0:MAXPRO),HEIGHT(0:MAXPRO),WIDTH(0:MAXPRO),	10
11		4 XSTOVE,YSTOVE,ZSTOVE,WSTOVE,HSTOVE,XWALL,YWALL,RTOTAL,QTOTAL,N,	11
12		5 IVAR,ISUB,VLOWER,VUPPER,VINCR,DEBUG,FULPRT	12
13		COMMON /CSTOVE/ MATL(0:MAXPRO),VNAME,TITLE	13
14	C		14

Appendix B: Data Input for STOVE

The data input for stove takes the form of six different key words with arguments to specify values which depend upon the key word. In most cases, the order of the key words is unimportant, except as noted below. A description of each of the input key words and values which go on the same line are presented below:

STOVE	<height> <width> <emissivity> <temperature>
AIRSPACE	<thickness> <emissivity>
FOR	<variable> = <lower> <upper> <increment>
XWALL	<x position>
YWALL	<y position>
PROTECTOR	<thickness> <height> <width> <k> <emissivity> <temperature>

BOLDFACE type are required key words. Words in <brackets> specify numeric inputs as follows:

<emissivity> specifies the emissivity of the cooler surface of the material. If specified for an airspace, it is the emissivity of the surface adjacent to the airspace at the farther distance from the stove.

<height> specifies the height of the stove or protector in meters.

<increment> specifies the amount to increment the variable <variable> in the **FOR** statement for each calculation to be performed. The first calculation is done with <variable> equal to the value <lower>; the second calculation is done with <variable> equal to the value <lower> + <increment> and so forth until the value of <variable> is greater than or equal to the value of

<upper>. The units for the number are the same as those for the variable <variable>.

<k> specifies the thermal conductivity of the solid protector in $W/m \cdot K$.

<lower> specifies the beginning value of the variable <variable> in the **FOR** statement for each calculation to be performed. The first calculation is done with <variable> equal to the value <lower>; the second calculation is done with <variable> equal to the value <lower> + <increment> and so forth until the value of <variable> is greater than or equal to the value of <upper>. The units for the number are the same as those for the variable <variable>.

<temperature> specifies the temperature of the stove surface, protector, or airspace in K. Temperatures are only specified for the stove surface (surface number 0) and for the outermost surface or airspace (surface number N).

<thickness> specifies the thickness of the material (for a protector) or the distance between surfaces (for an airspace).

<variable> specifies the variable to be incremented in each calculation to be done. The first calculation is done with <variable> equal to the value <lower>; the second calculation is done

with <variable> equal to the value <lower> + <increment> and so forth until the value of <variable> is greater than or equal to the value of <upper>. Legal variables which may be used are: T(0) -- the stove temperature, width(i), k(i), xwall, ywall, emissivity(i), height(i), l(i).

<width> specifies the width of the stove or protector in meters.

<x position> specifies the x position of the point on the wall at which the calculation is to done in meters.

<y position> specifies the y position of the point on the wall at which the calculation is to done in meters.

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10. SUPPLEMENTARY NOTES <input type="checkbox"/> Document describes a computer program; SF-185, FIPS Software Summary, is attached.			
11. ABSTRACT (A 200-word or less factual summary of most significant information. If document includes a significant bibliography or literature survey, mention it here) A computer implementation of a model to predict temperatures on wall and wall protector surfaces exposed to the heating of an appliance such as a solid fuel heating appliance is described. A steady state heat transfer model with flexibility to describe a generalized method of protection for a combustible wall surface is presented along with a computer program implementing the model. Good agreement was found comparing the model predictions with data previously collected during full scale experiments conducted to evaluate the effectiveness of generic methods of wall protection in reducing temperatures on combustible wall surfaces. Extensive references of research related to solid fuel heating safety are included.			
12. KEY WORDS (Six to twelve entries; alphabetical order; capitalize only proper names; and separate key words by semicolons) chimneys; fire models; fire safety; fire tests; flues; heat transfer; heating equipment; literature reviews; radiant energy; stoves; wood			
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